

Advanced Concentrating Thermal Technologies for Power and Process Heat Generation

Robert Pitz-Paal



Knowledge for Tomorrow

Outline

1. Characteristics of CSP
2. Market und Cost Development
3. Benefits for a mix of PV und CSP
4. Process Heat
5. Advances Heat Transfer Fluids
 - Volumetric Air Receiver
 - New silicon oil heat transfer fluid
 - Molten salt in parabolic troughs
6. Conclusions

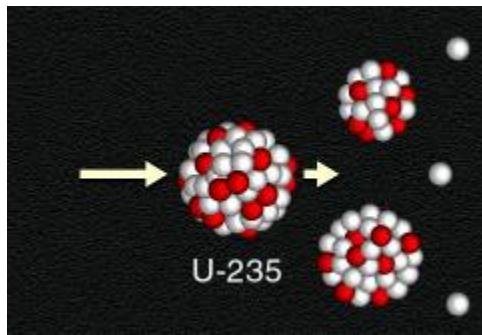


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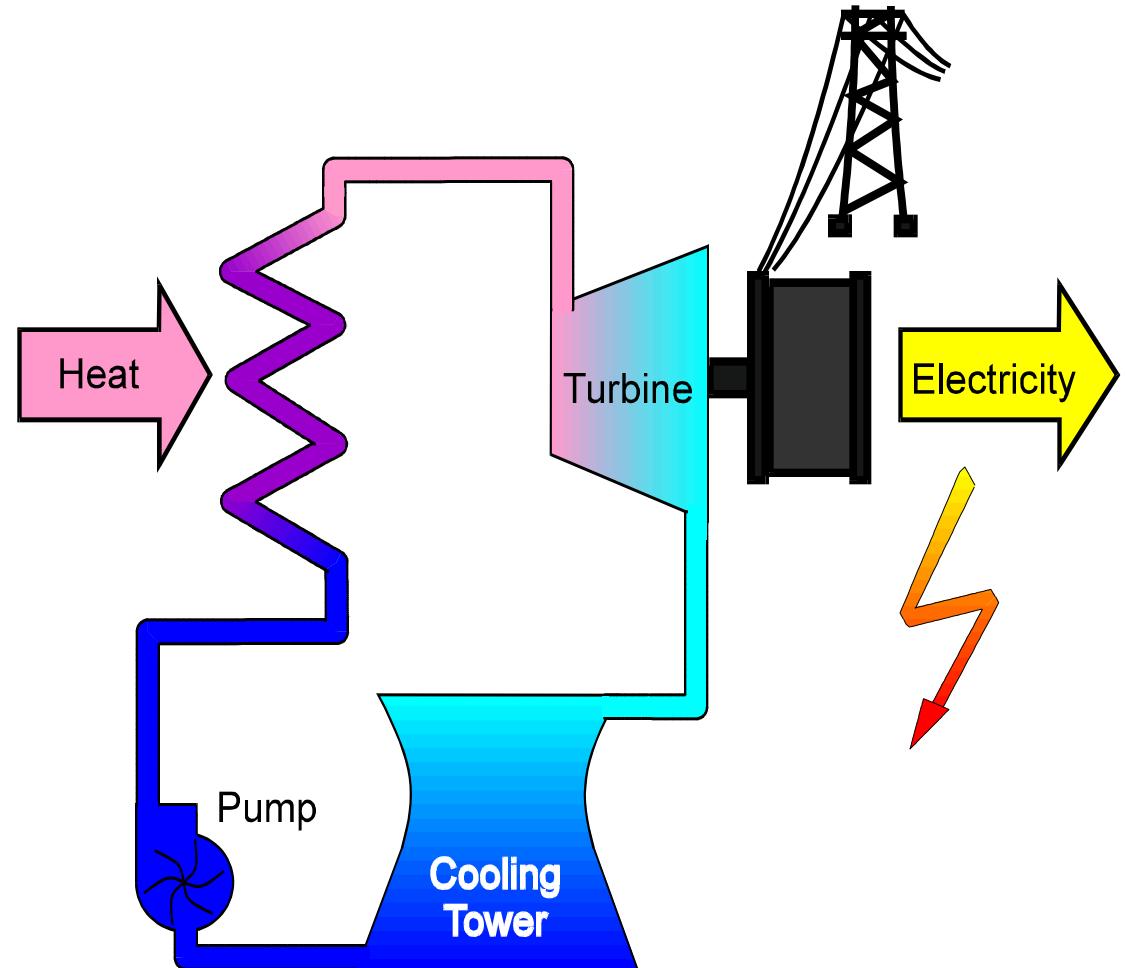
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What is CSP?



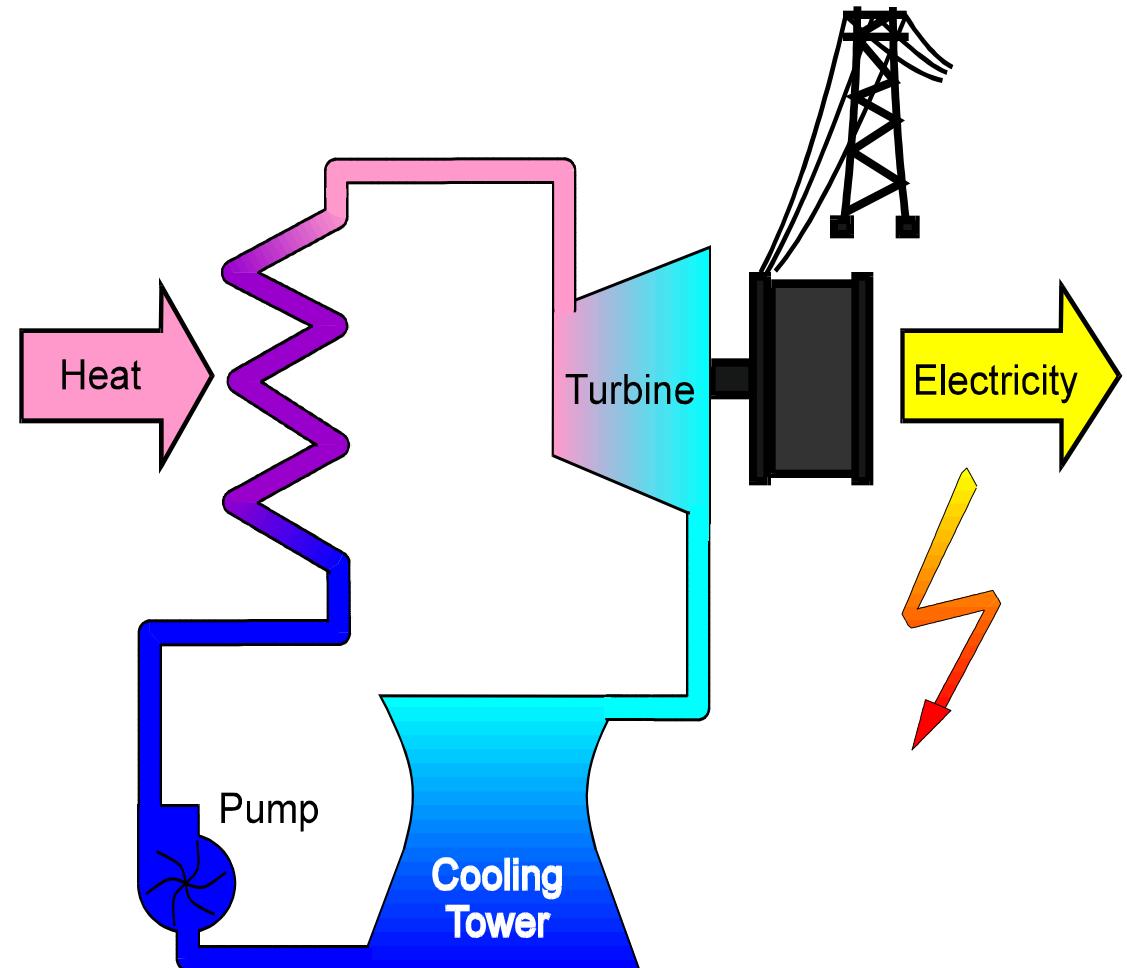
Conventional power plant



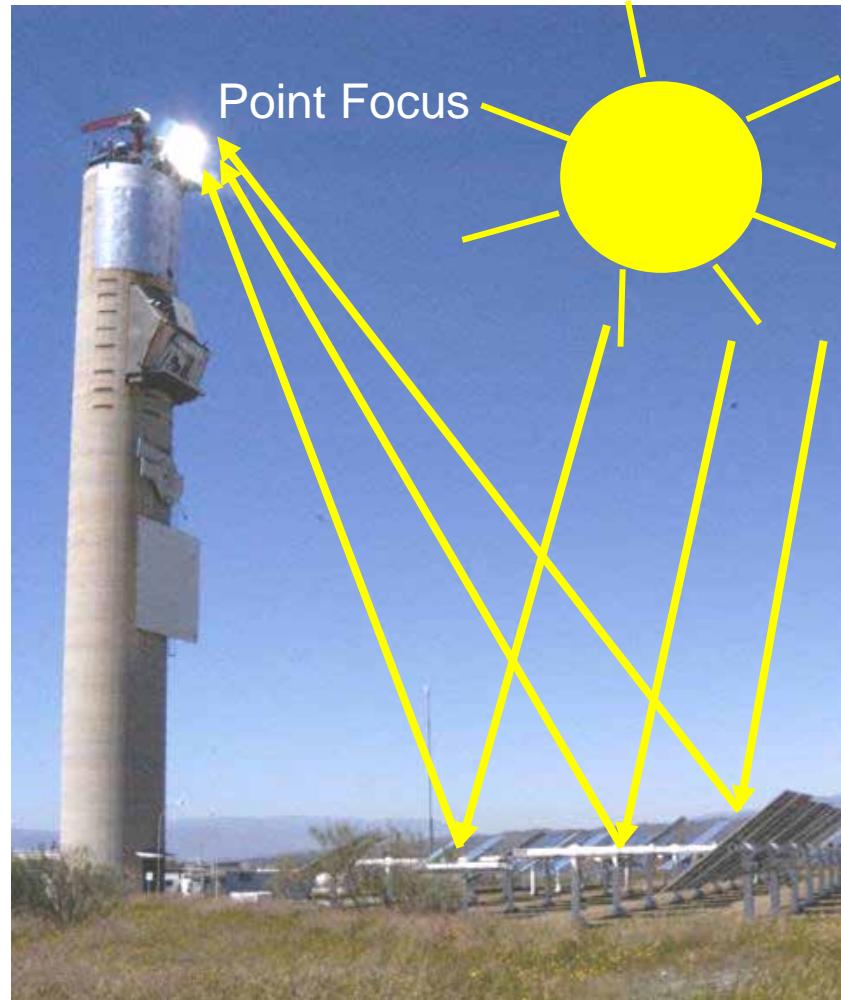
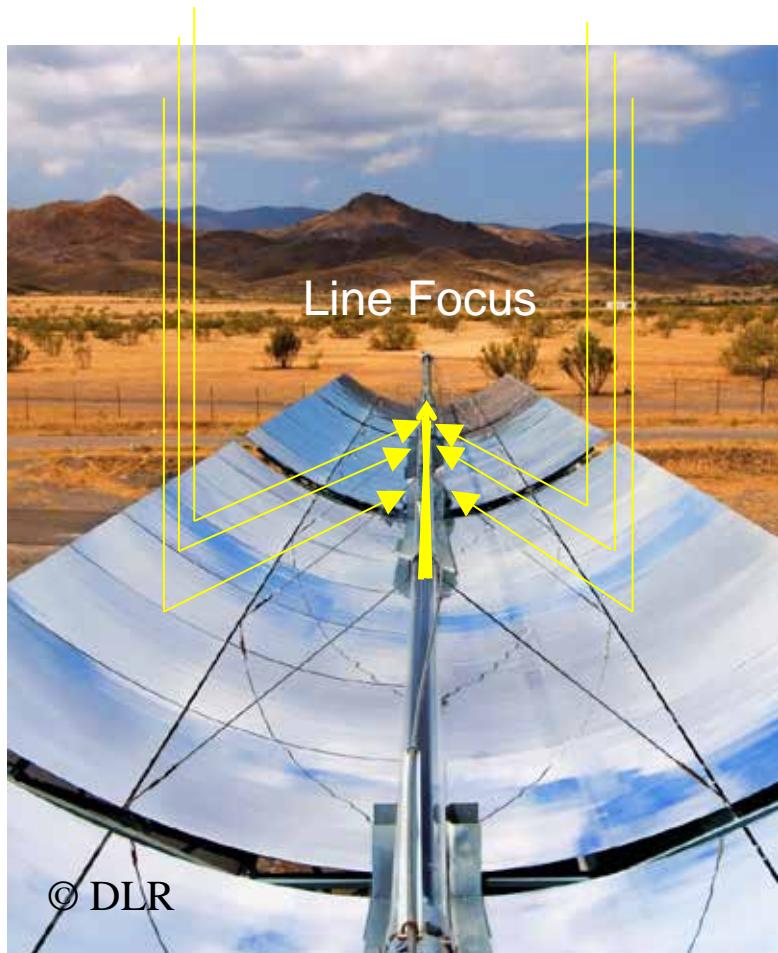
What is CSP?



Concentrating solarpower plant

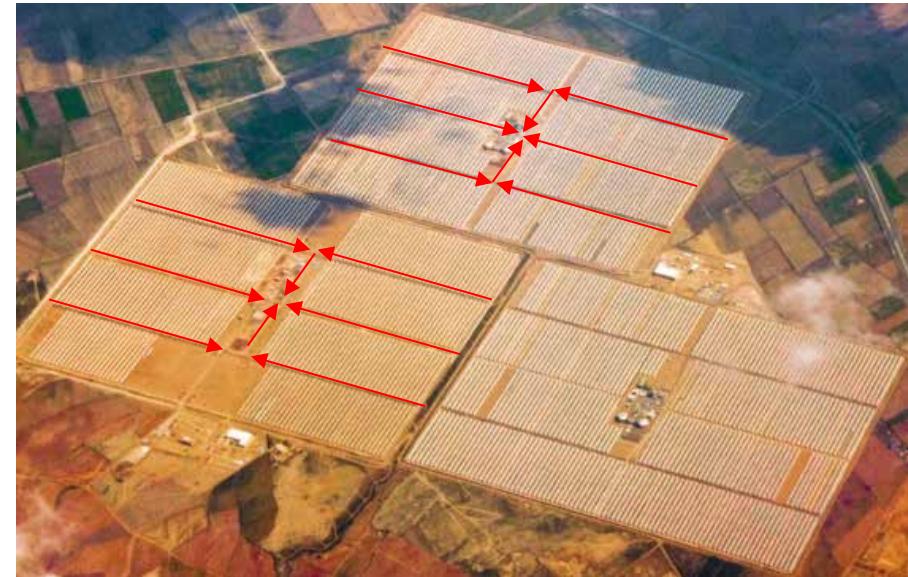


Trough vs. Tower

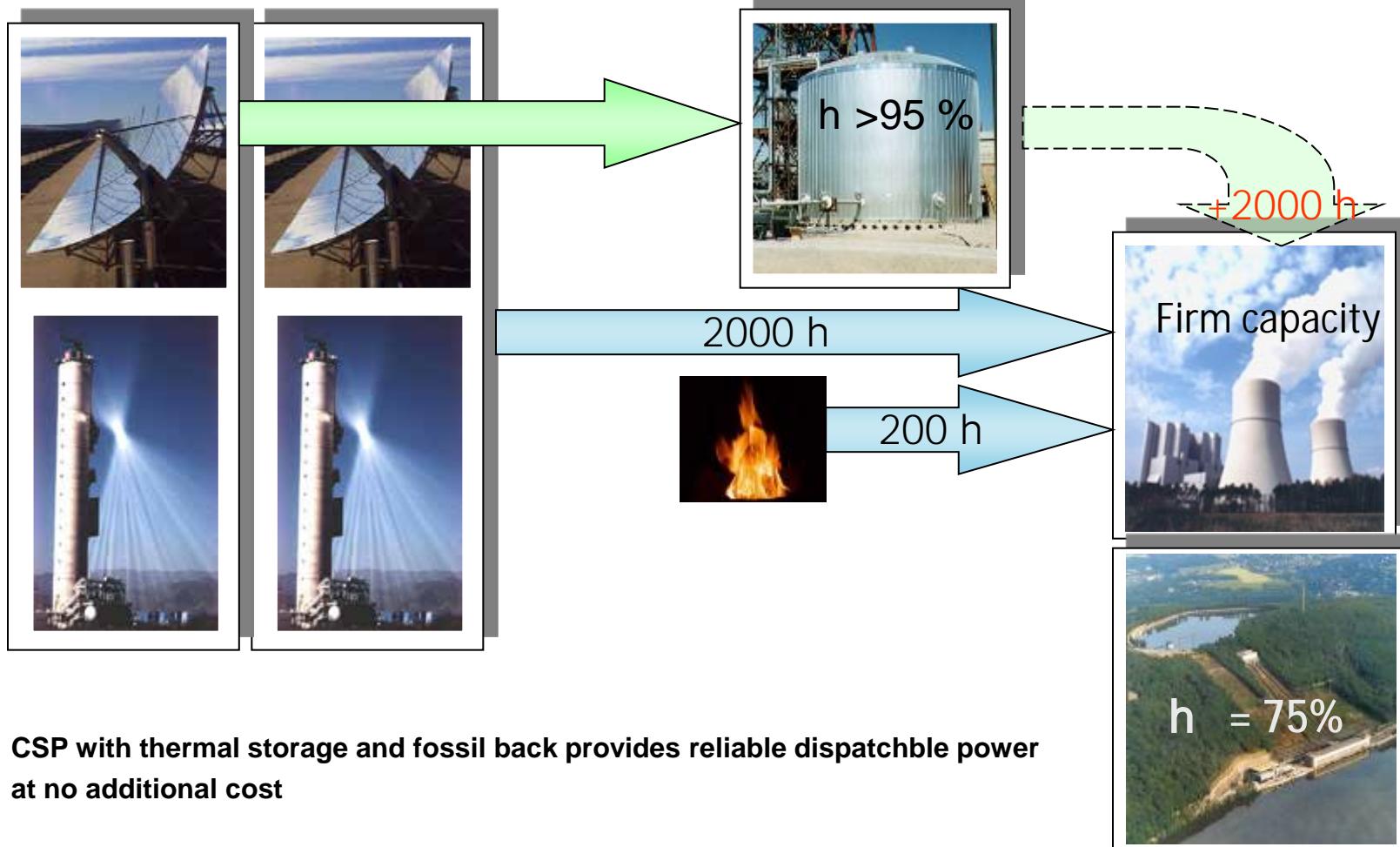


Trough vs. Tower

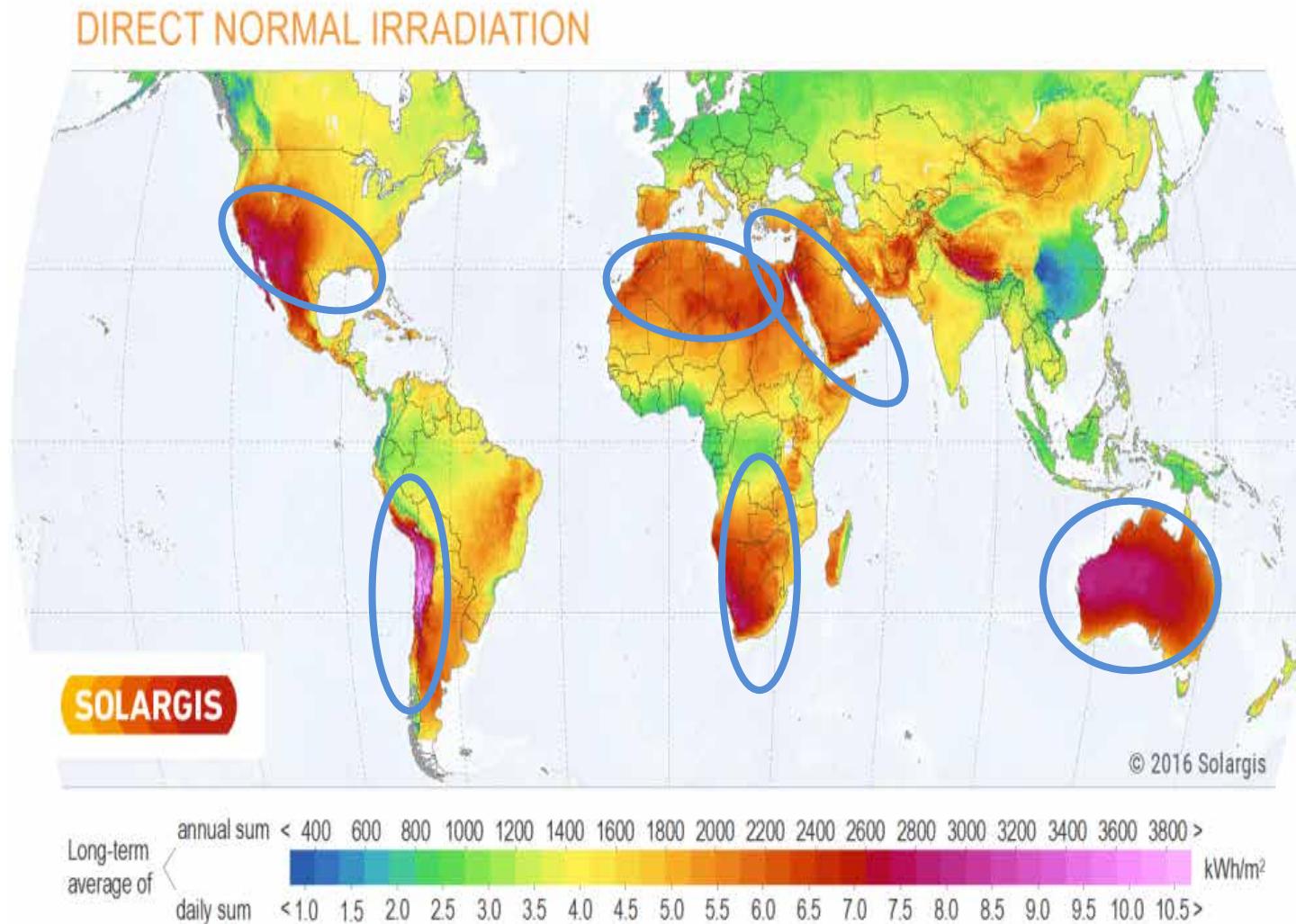
- Solar energy collected by reflection
- Solar energy collected by piping



Thermal Storage vs. Electric Storage



CSP only suitable in areas with high direct normal radiation

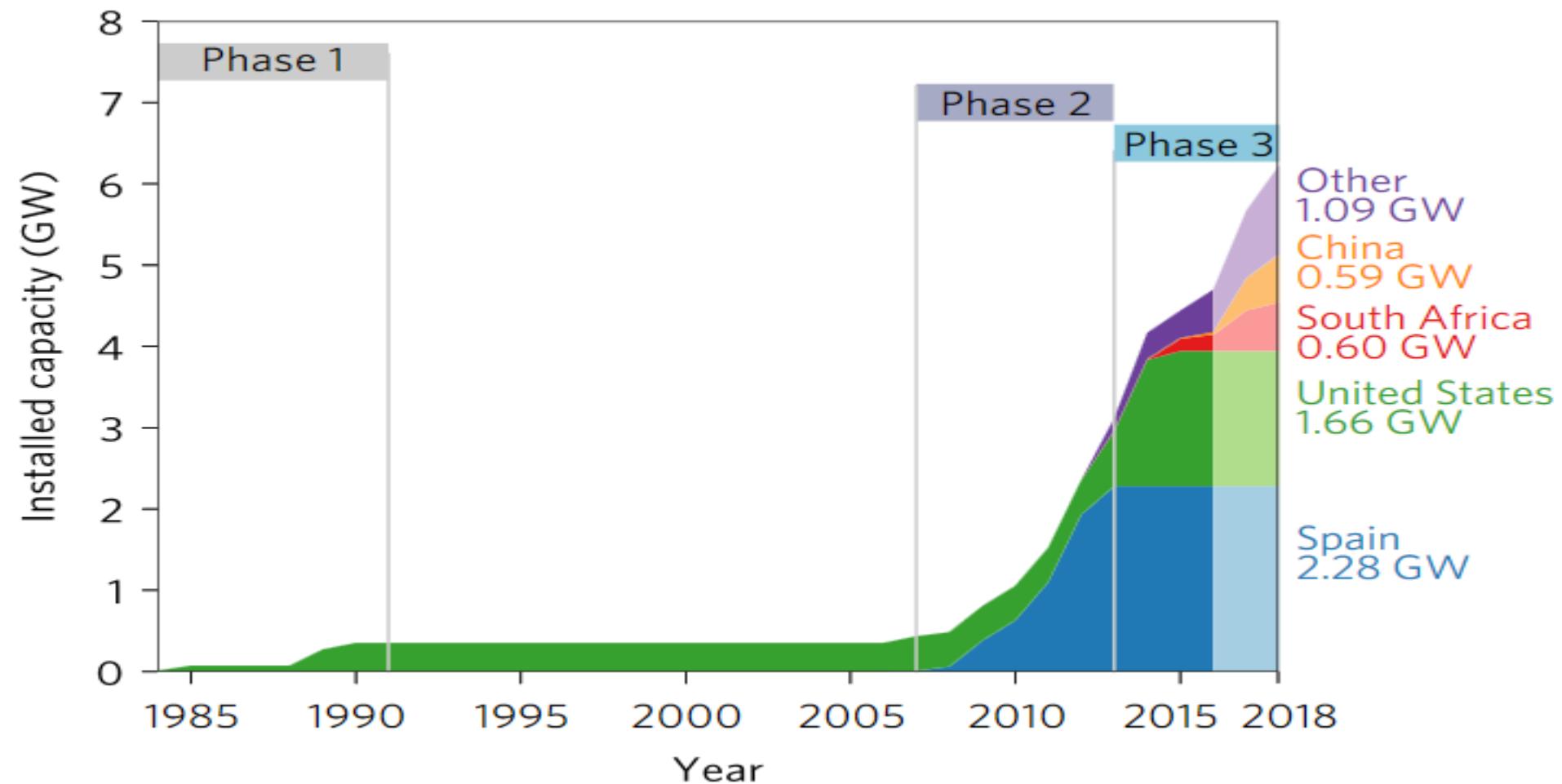


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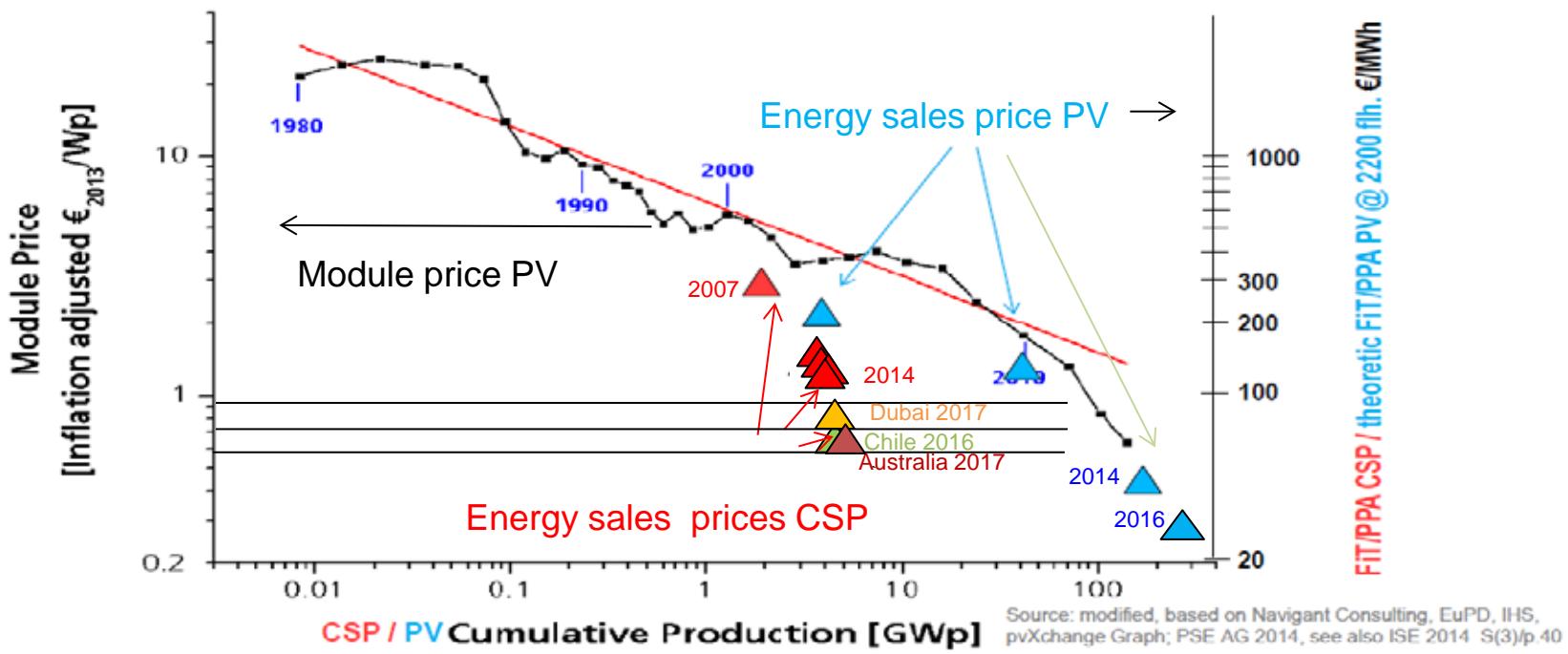
Global expansion of CSP in three phases



Lilliestam, J., Labordena, M., Patt, A. & Pfenninger, S.
Nat. Energy 2, 17094 (2017).

Cost for CSP and PV have dropped dramatically

- Installed CSP capacity is more than an order of magnitude smaller than PV capacity



DEWA IV Project – Largest CSP project in the world at 7,3 cent/kWh

Solar Electricity cheaper than power from gas!

700 MW @ 5500 h CSP á 7,3 \$cents/kWh

+ 800 MW @ 2300 h PV a 3 \$Cents/kWh

$$= 5,95 \text{ $cents/kWh}$$

$$= 5,07 \text{ €cents/kWh}$$

for 24/7 electricity

4

Football fields

Source: ACWA POWER

Designed to dispatch base load electricity on a 24 hour basis, with embedded flexibility of operation to address the Dubai load profile depending on seasons.

- 100 MW CSP Molten Salt Tower with 15 hours of storage
- 3 x 200 MW CSP Parabolic Trough with over 10 hours of storage

More than

5000 full load hours

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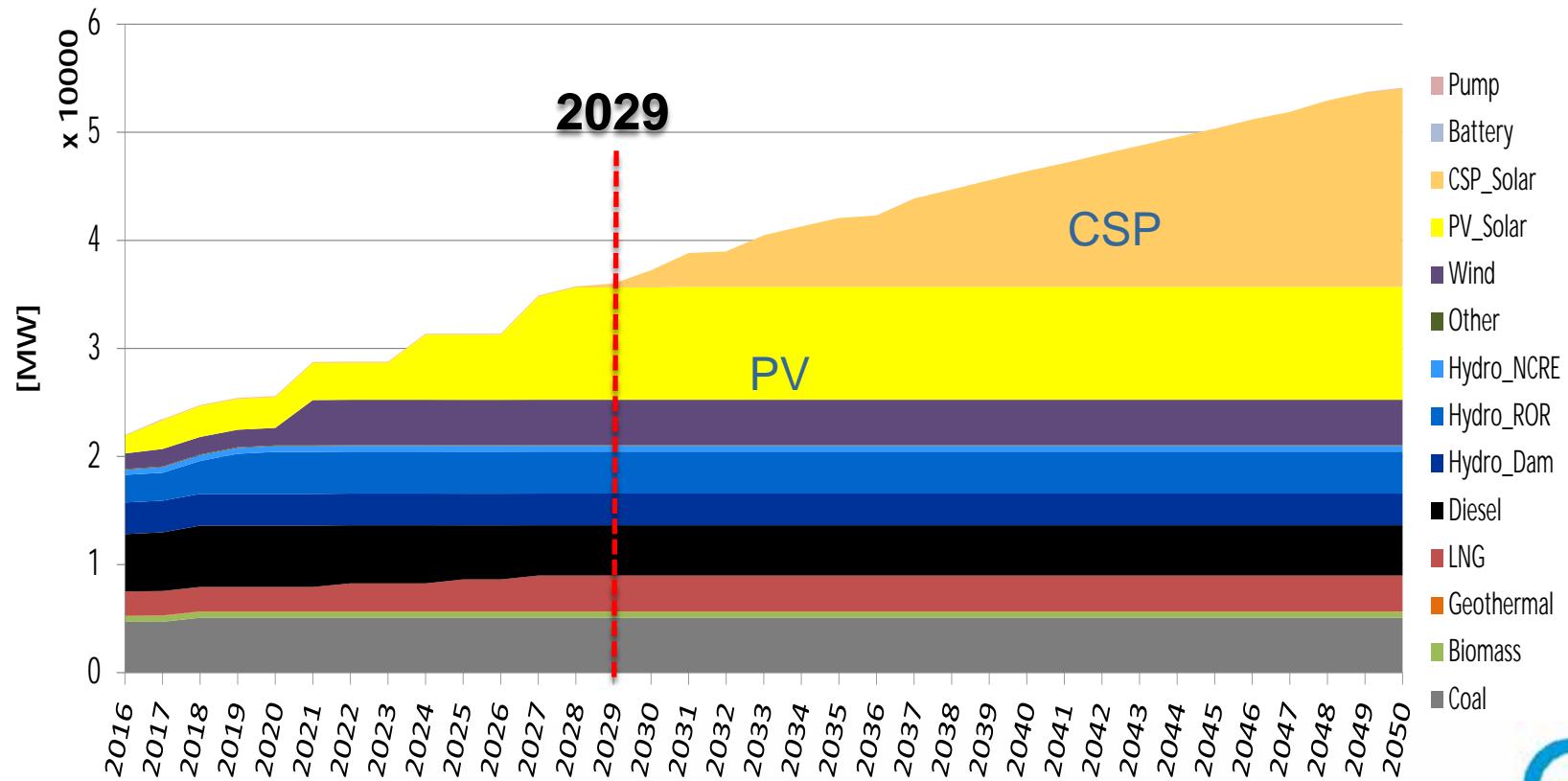


Chile Scenario Results – Expansion Model

Scenario 1

	Social acceptance	Energy demand	Technological change in BESS	Externality costs	RE investment costs	Fossil fuel costs	CSP LCOE
Scenario B	High	High	Low	High	Low	High	USD 50 /MWh by 2025

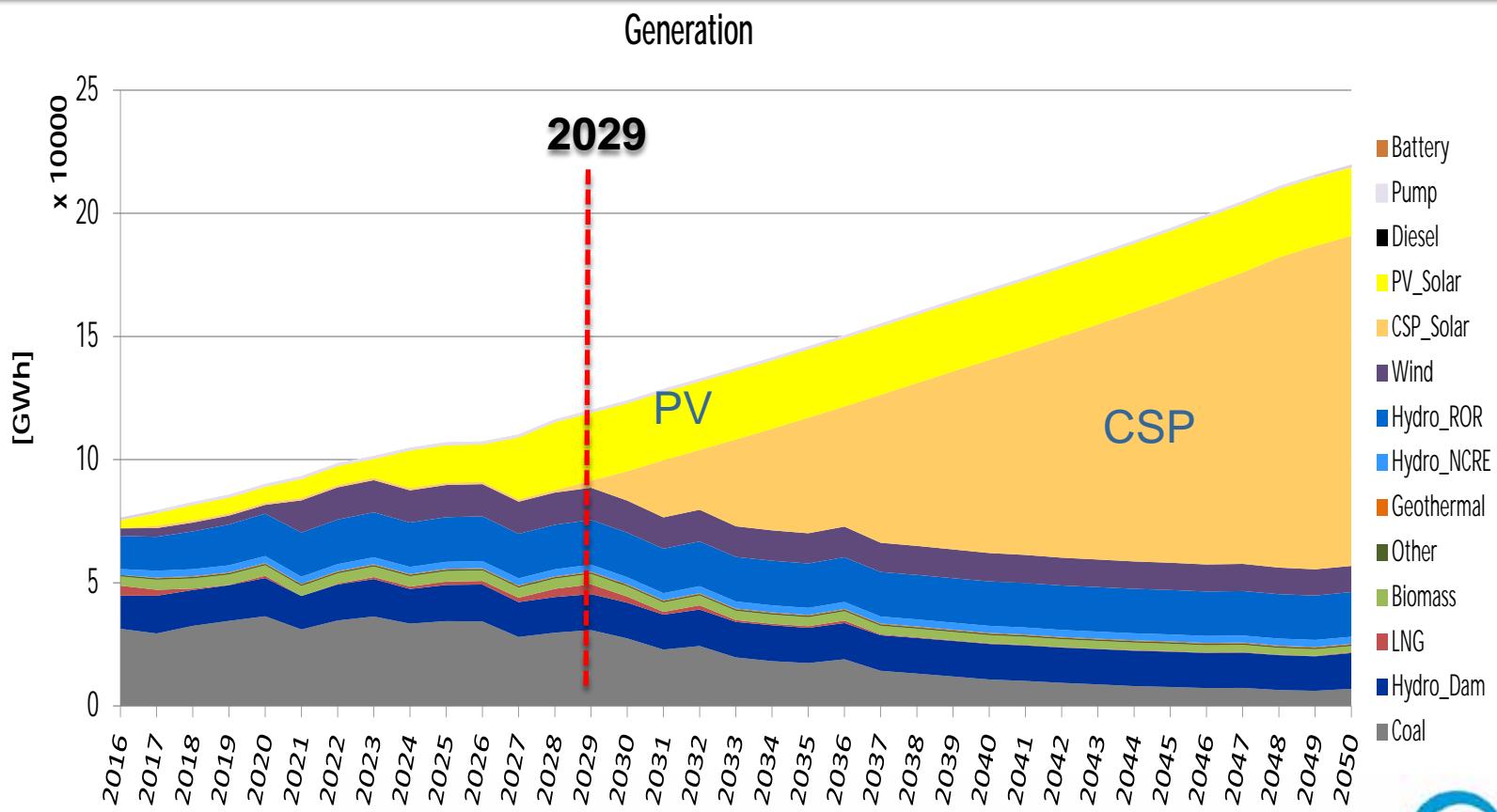
Installed Capacity



Chile Scenario Results – Expansion Model

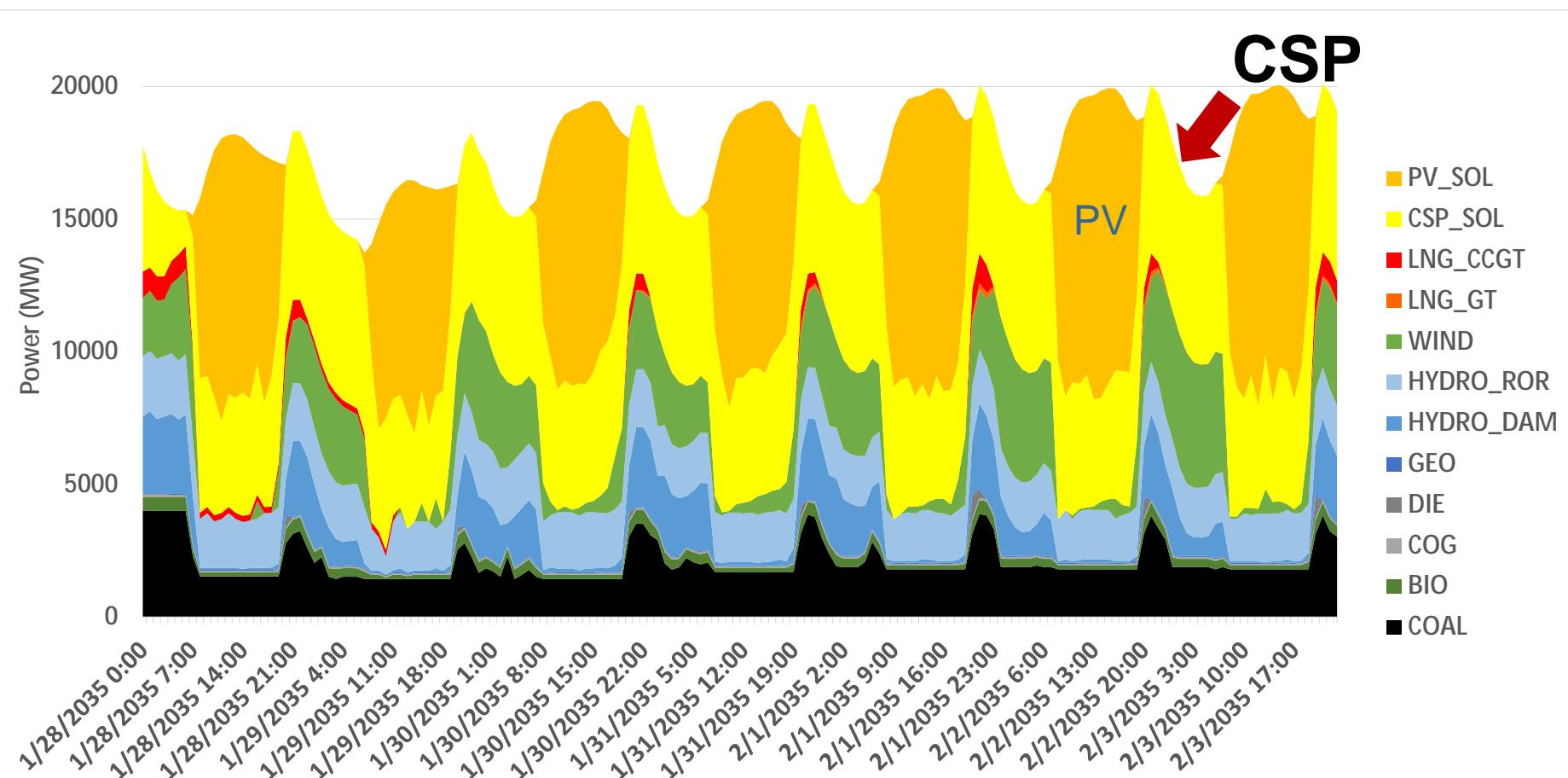
Scenario 1

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Chile Szenario results: Short Term Simulation

2035 summer week dispatch by technology



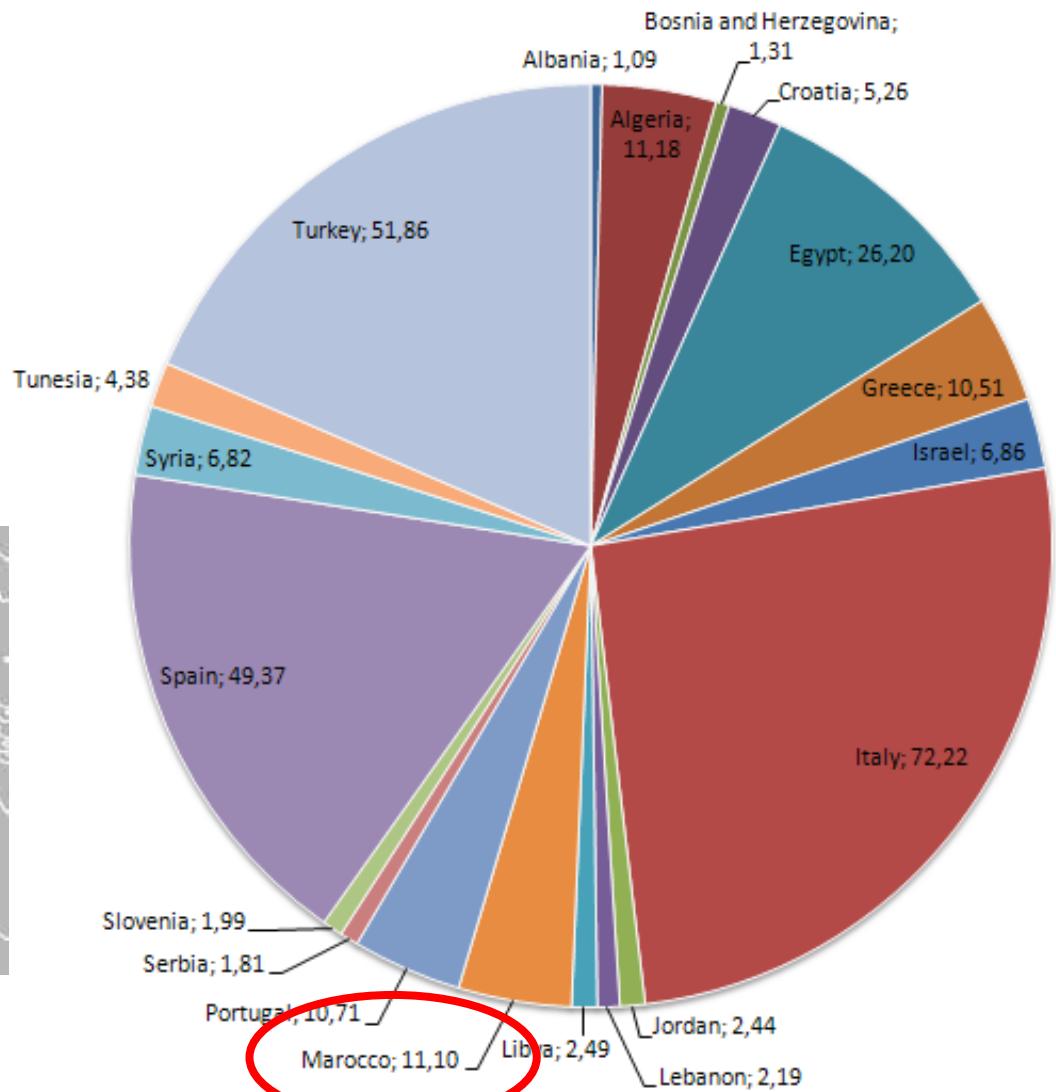
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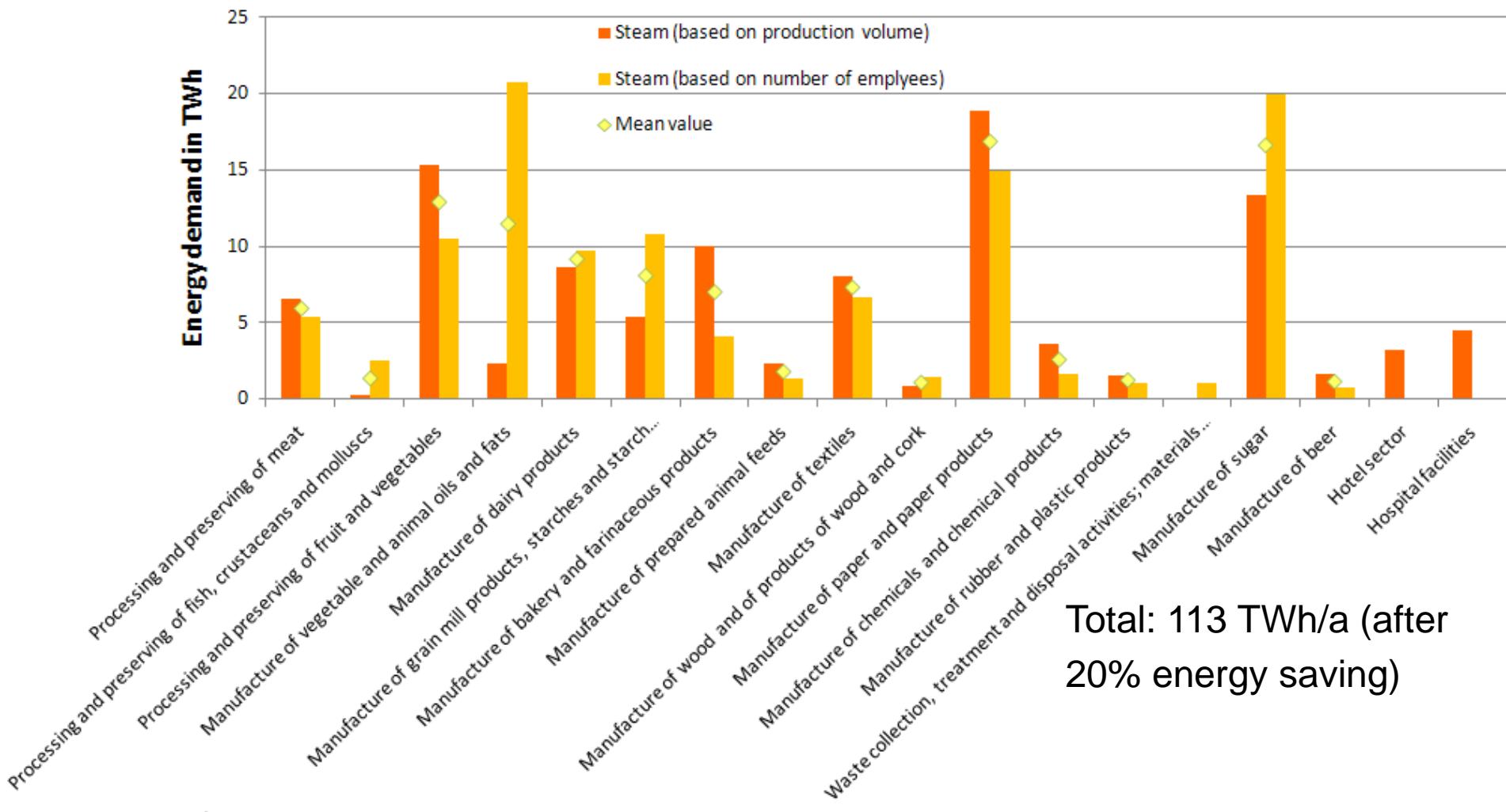


Process Heat Demand in Mediterranean Countries

Total Process Heat Demand
280 TWh/a
after 20 % energy savings



Process Steam Demand by Industry Sectors



Challenges in Solar Process Heat

- Heat cannot be transported easily over long distances
 - Meteorological conditions at the site
 - Availability of suitable areas for collectors (ground, roof, facades)
- Solar field size (= investment cost) proportional to heat demand
 - Rational use of energy minimizes heat demand
 - Process optimization more cost effective than “free” solar energy
- Collector efficiency temperature dependent
 - Selection of suitable collector technology
 - Integration of solar heat at appropriate temperature
- Annual, daily and stochastic variations of radiation
 - Load management, heat storage or conventional back-up
 - Similar load and radiation profiles may increase solar share
- O&M effort for additional technology
 - Priority for O&M personnel: Efficient production
 - Fully automated solar operation



Example: Solar Process Heat, Saignelieger, Switzerland

- **NEP Solar:** Cheese factory in Saignelégier, Switzerland.
- 17x NEP Solar PolyTrough 180 collectors Commissioning Sept. 2012
- Hot water/antifreeze circuit , 130 ° C
- 627m², 400kW nominal heat capacity



Example Process Heat, New York City

- Steinway and Sons
- Long Island City, New York, USA
- Operational 2010
- 501 m²
- Back-up by natural gas
- Heating and cooling, process steam
- Humidity control of piano „action“ department



Example: Solar Process Heat at RAM Pharma, Amman, Jordan

- Solar field: linear Fresnel collectors of Industrial Solar GmbH
- Supply of saturated steam at 6 bar gauge
- Start of operation: March 2015



Collector field and steam drum with piping to steam network

Economic Example for Jordan

Parameter	Value	Comment
Fossil Steam Generation Cost in 2017	81.7 €/MWh _{th}	Only running cost; boiler efficiency 80%; ex. Rate 0.75 JOD/€
Turn-Key Investment Cost	766 000 €	i.e. 435 €/m ² (Industrial Solar costs – 10% incentives)
Running Cost per year	12 000 €	+1% per year
Equity Ratio	20%	
Debt Ratio	80%	
Debt term	10 years	
Debt funding interest rate	4%	

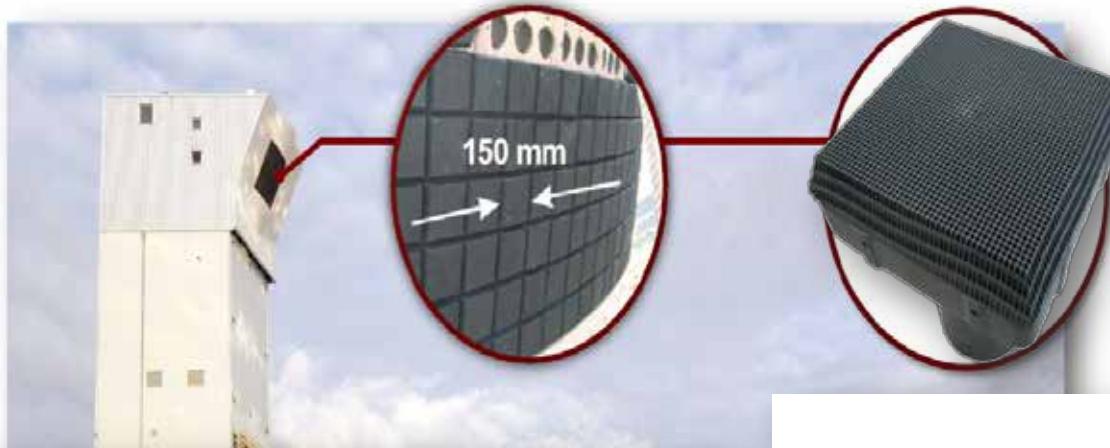
Economic Key Results	Base Case	6% Interest	100% Equity	
Payback Time	2.3	2.7	4.8	Years
Internal Rate of Return (IRR)	52	47	23	%
Levelized Heat Cost	41.4	41.4	41.4	€/MWh _{th}

Outline

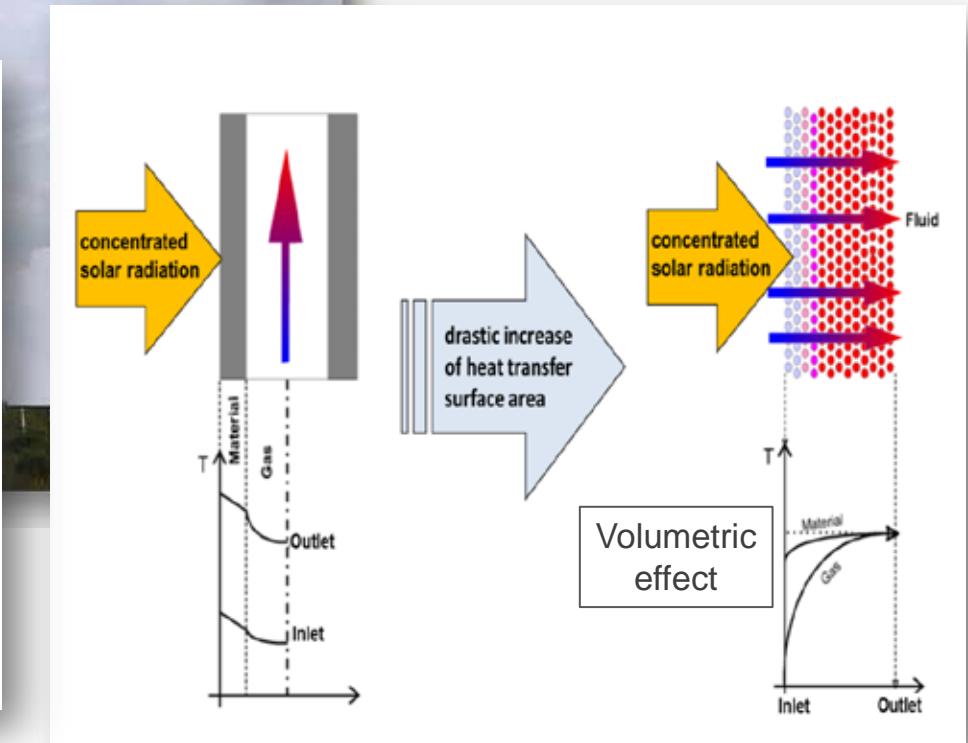
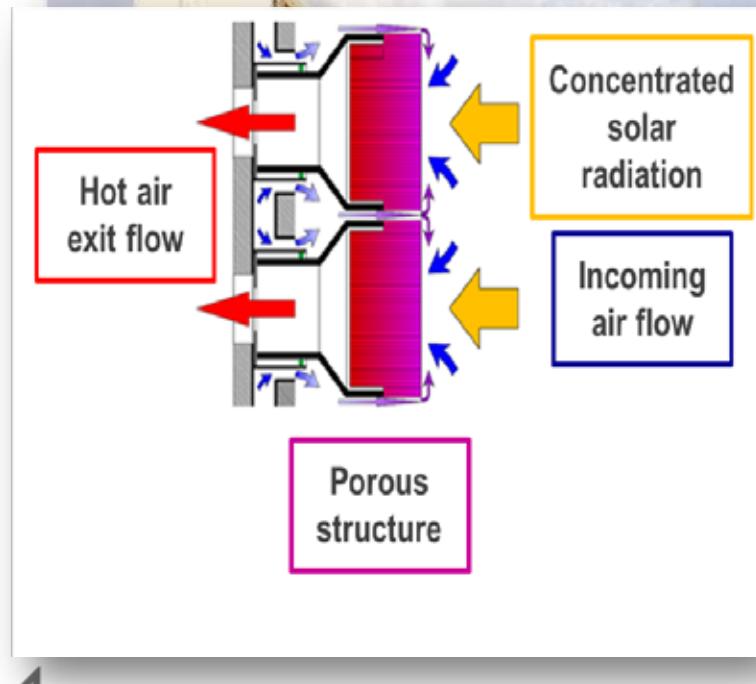
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Energy from the sun: Open volumetric solar receiver



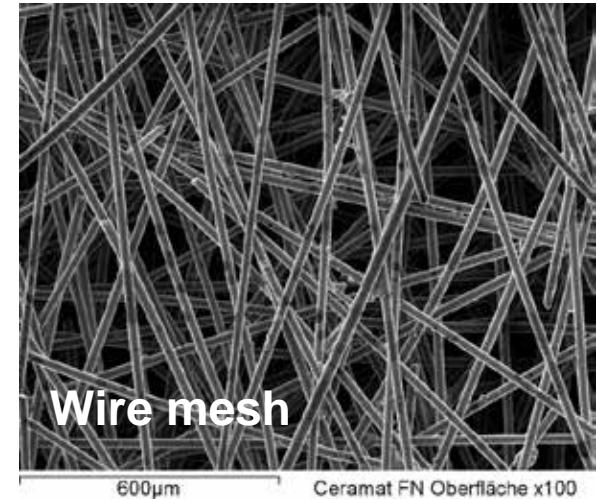
HiTRec-II
SiSiC
honeycomb



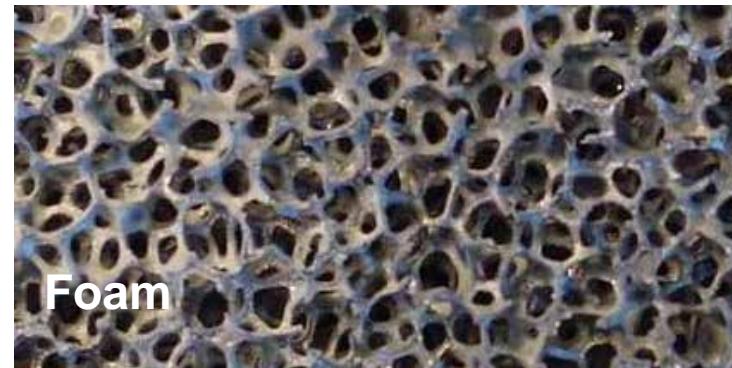
What is the perfect absorber?



Honeycomb



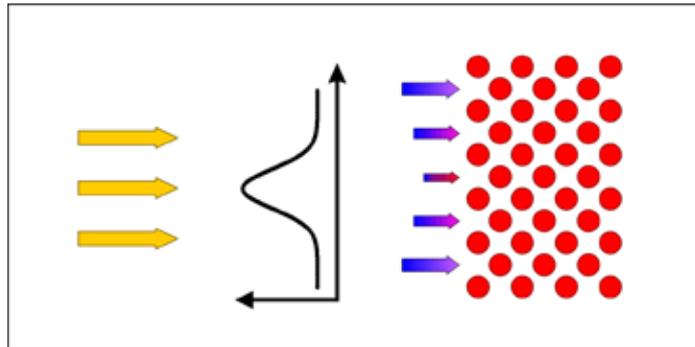
Wire mesh



Foam



Different Characteristics affecting Flow Stability



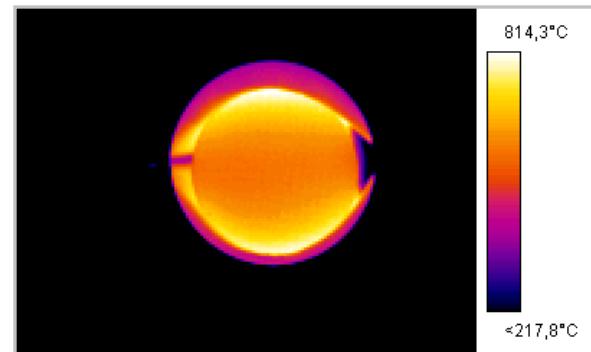
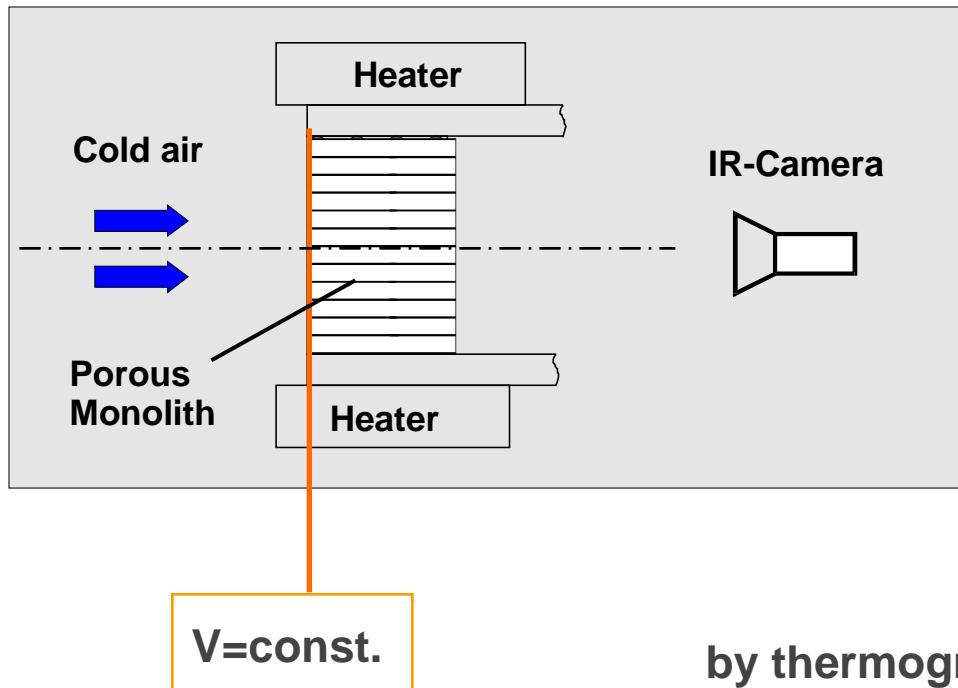
- ↗ viscosity increases with increasing temperature
- ↗ hot zones are badly cooled



- ↗ local hot spots
- ↗ ® instable flow at
 - high temperatures
 - linear pressure drop characteristics
 - low thermal conductivity

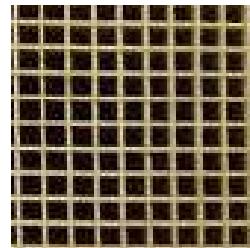


How can instable flow be visualized?

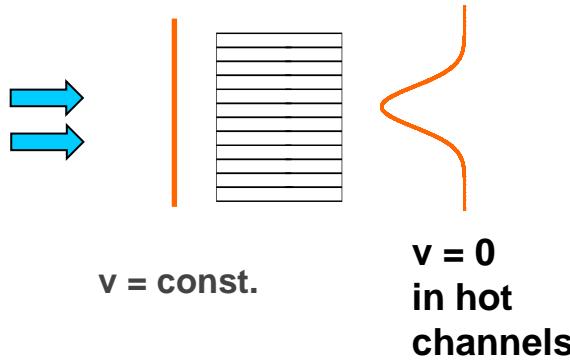
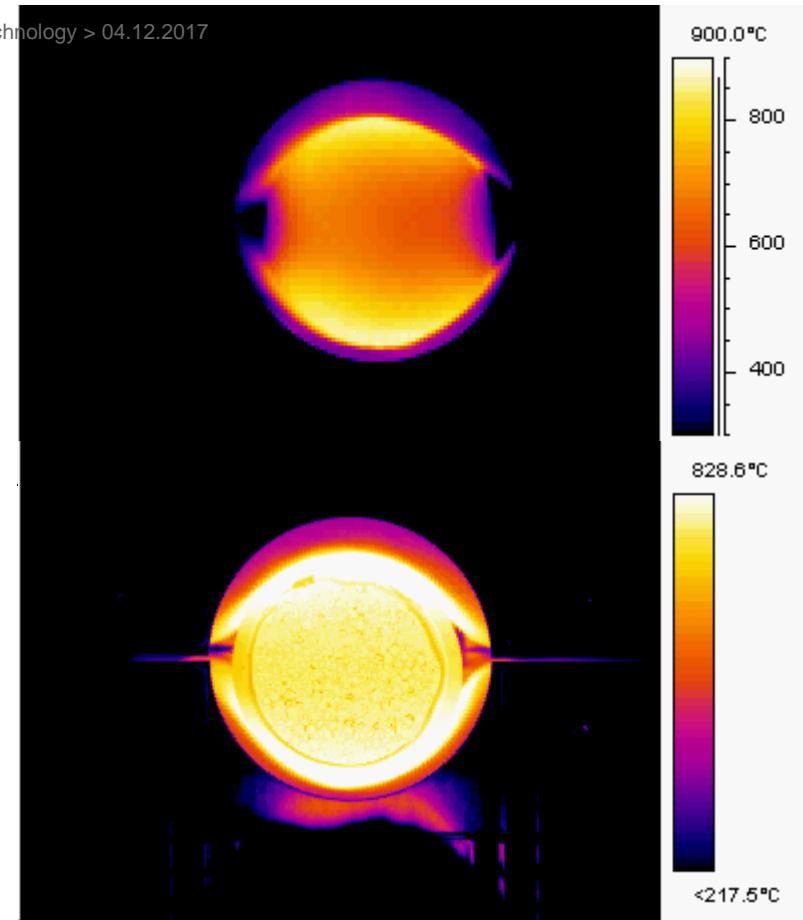


by thermograph monitoring of
the cooling of a heated porous monolith

**cordierite
honey
comb**



**SiC
foam**

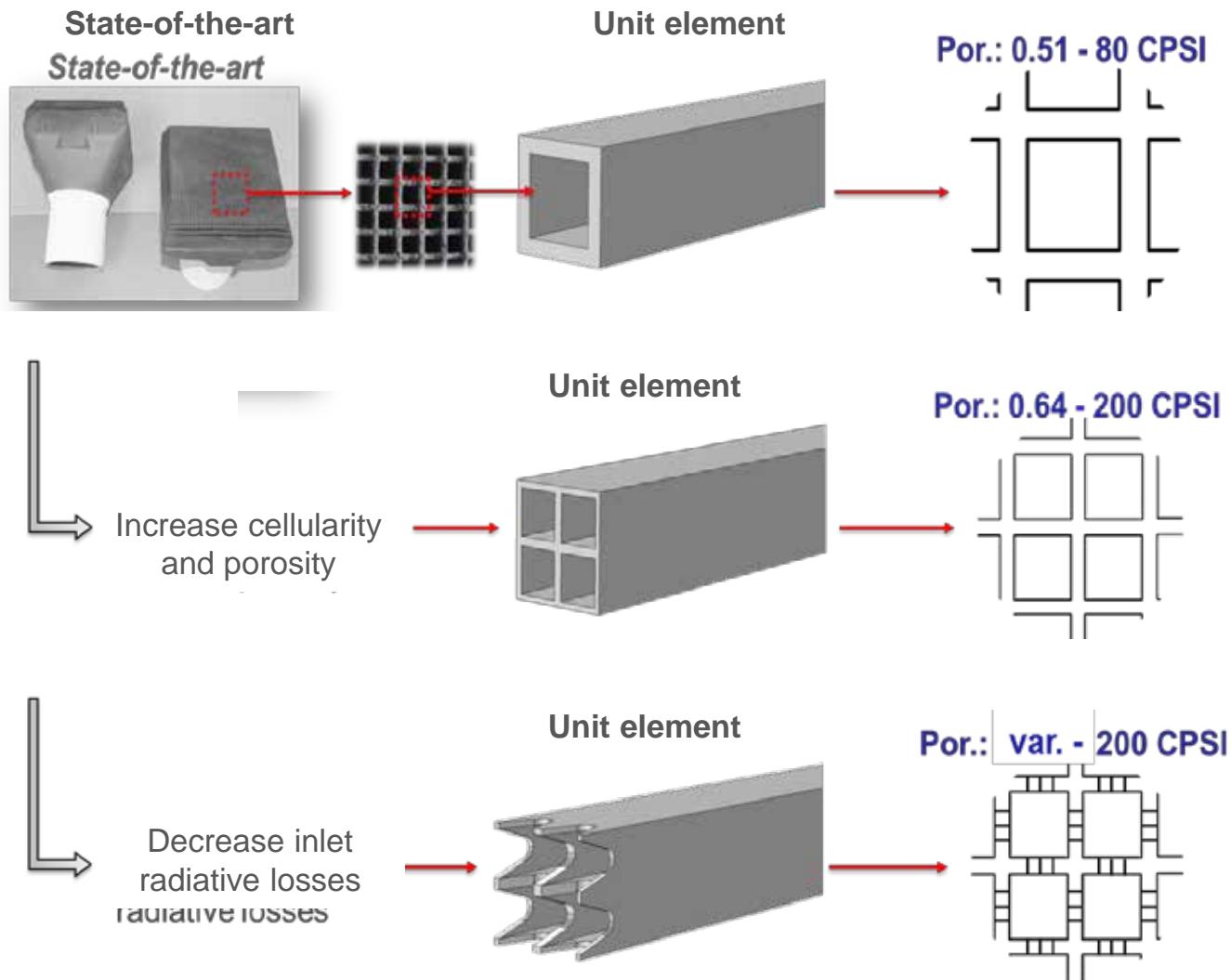


**geometry/pressure loss
characteristics influences
flow stability**



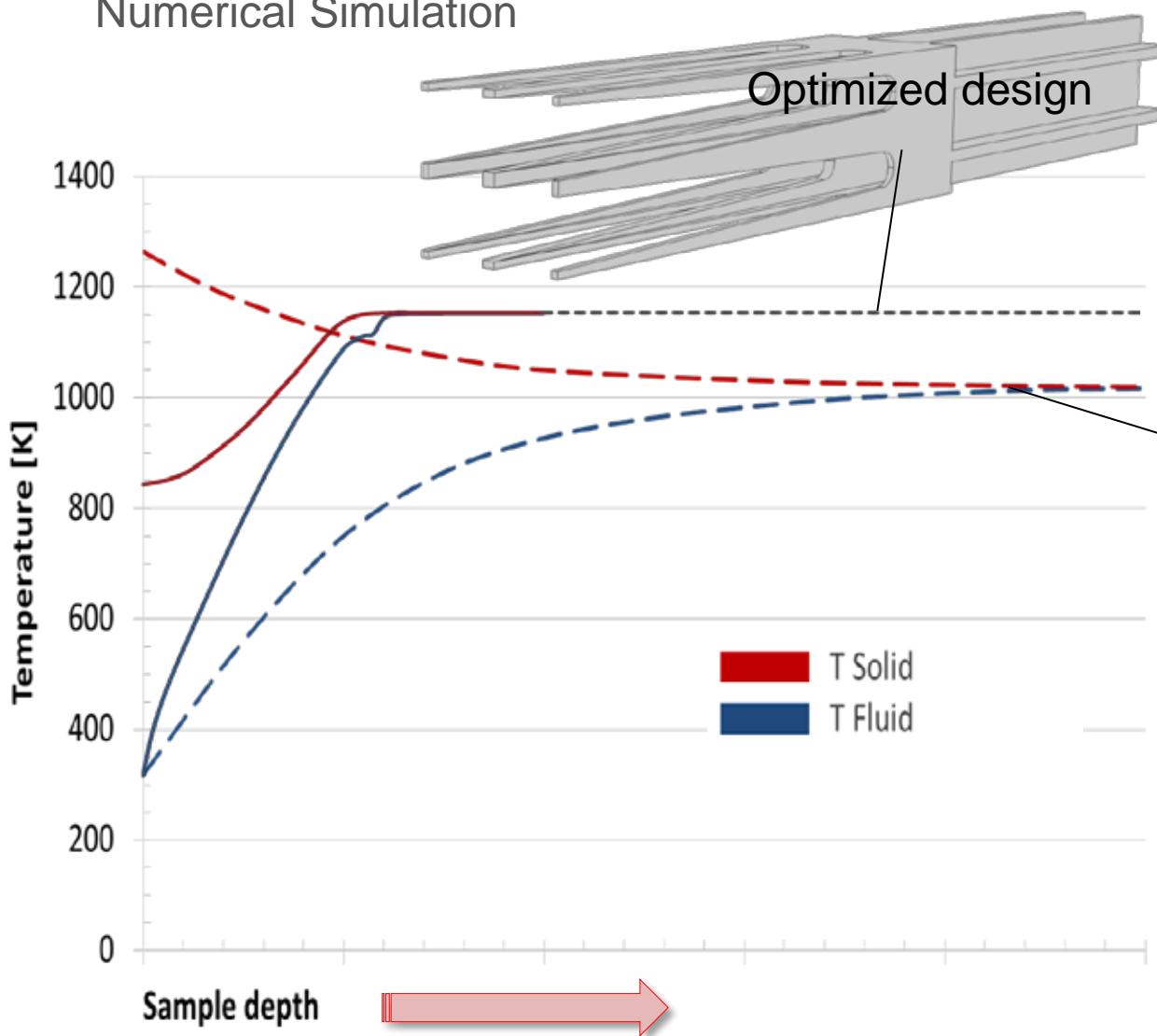
**heat conductivity influences
flow stability**

Optimizing the Absorber Design



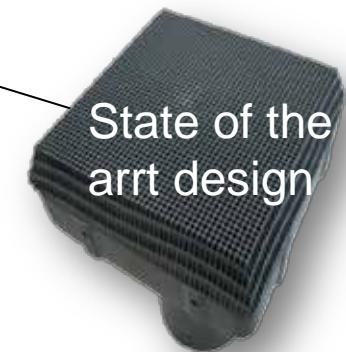
Optimizing the Absorber Design

Numerical Simulation



Innovative geometry

$T_{\text{air-out}}: 1149 \text{ K}$
 $\eta = 90 \%$



State of the arrt design

HiTRec-II

$T_{\text{air-out}}:$
1012 K
 $\eta = 72\%$



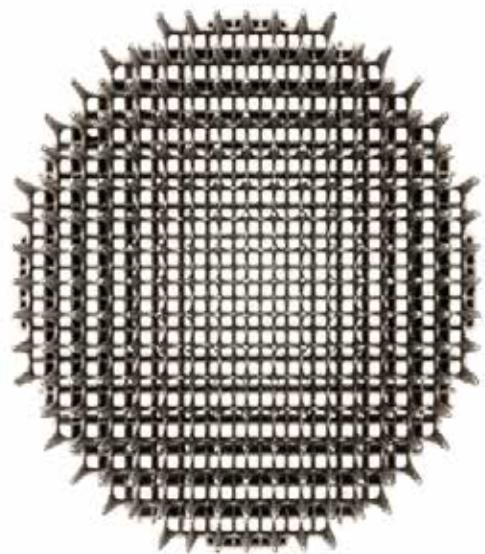
Prototype sample production by 3D printing

Cylindrical prototype test-sample: Ti6Al4V 3:1 scaled up geometry

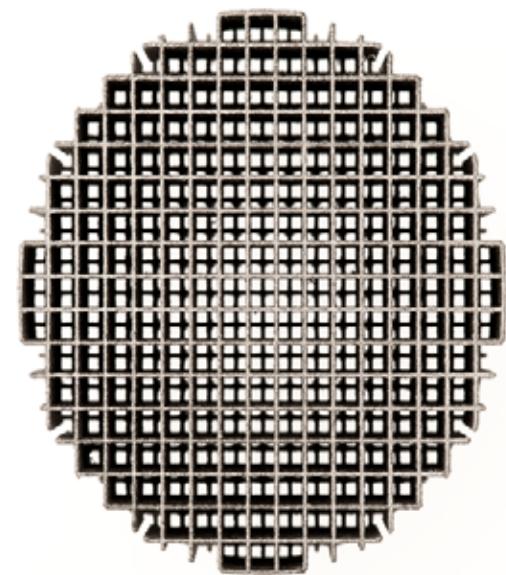
Front view



Top view

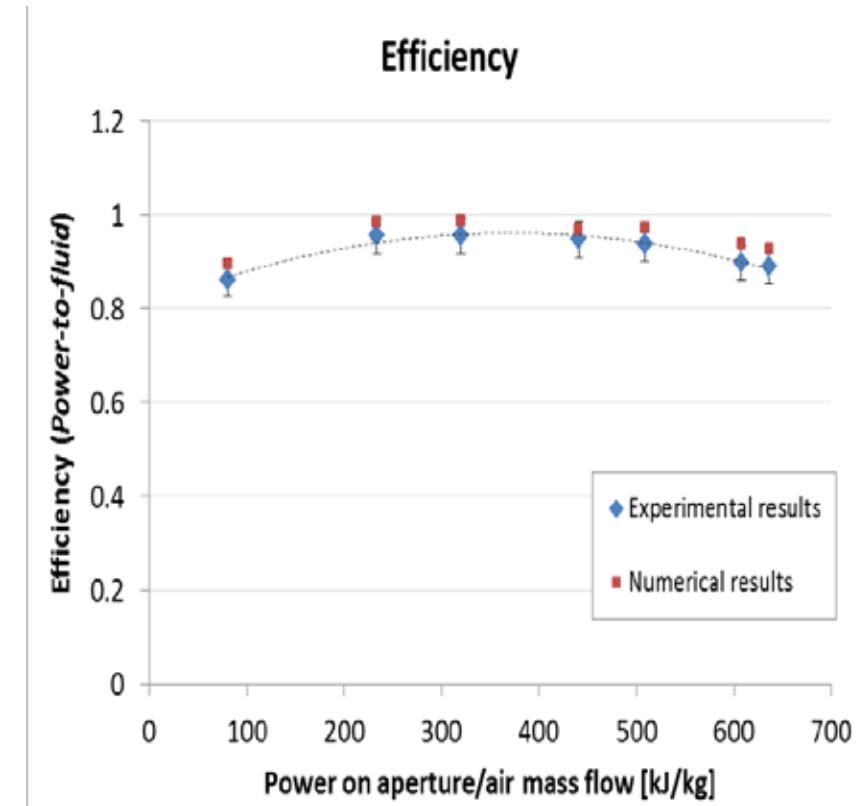
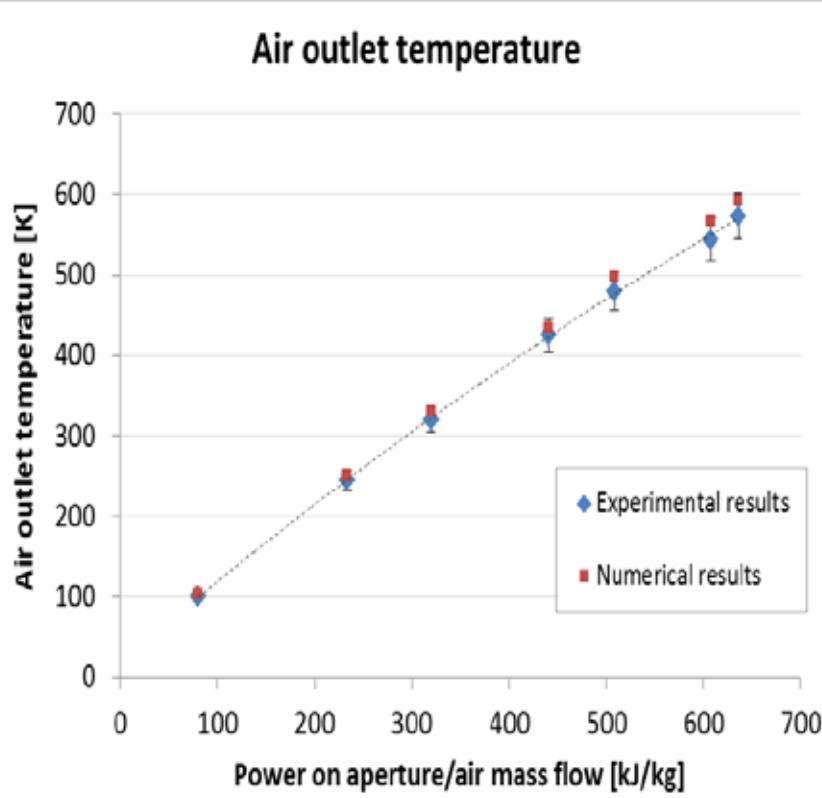


Bottom view



Experimental Validation of Prototype

Thermal efficiency evaluation à 20 kW solar simulator



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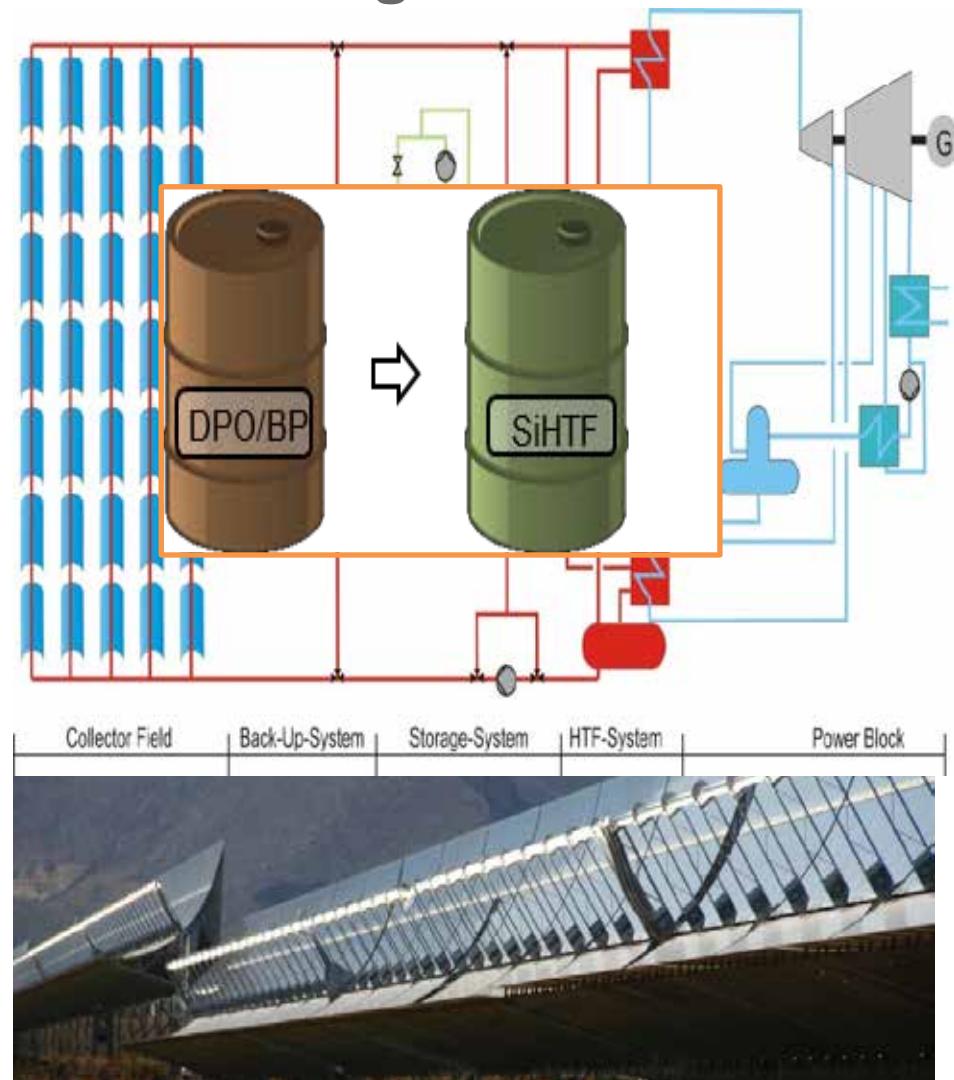


Advanced Silicon Oil in Parabolic Troughs

Ü Environmental Safety

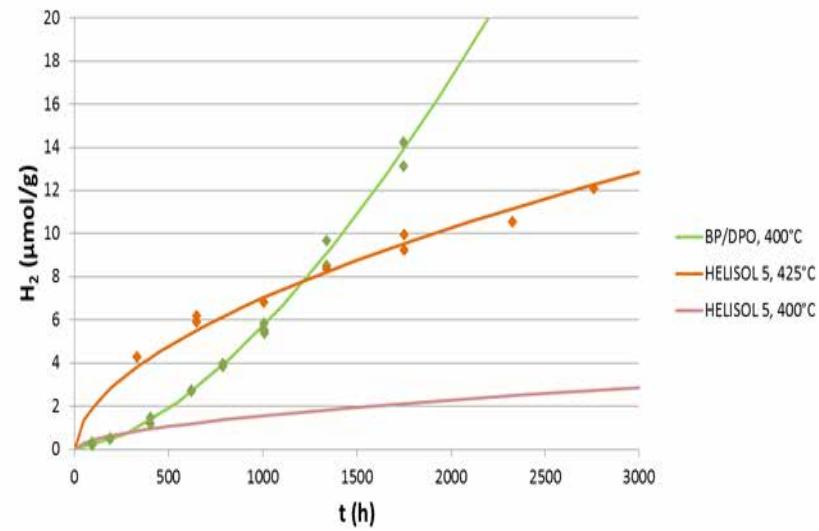
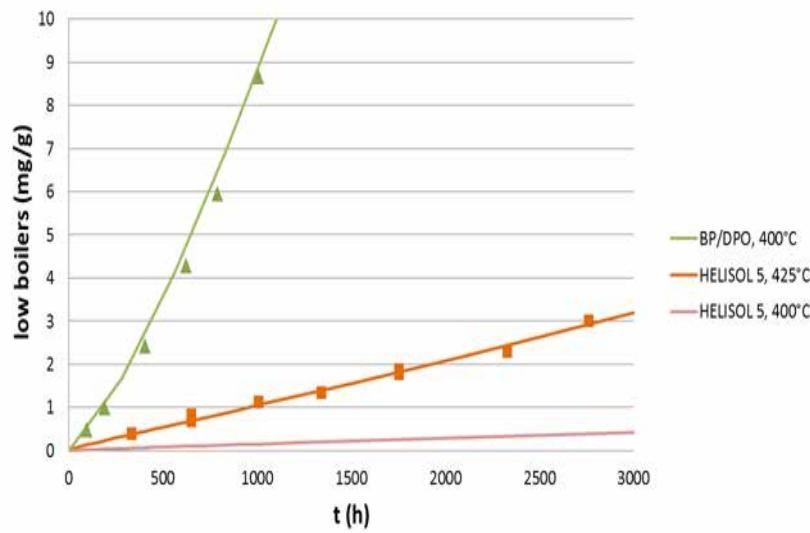
Ü Capacity / Performance

- *low pour point (-55°C) reduces auxiliary consumption for freeze protection*
- *slower degradation at 425°C in comparison to DPO/BP at only 400°C*
- *425°C field outlet temperature increases conversion efficiency of Rankine cycle and allows for smaller heat storage systems*



Advanced Silicon Oil in Parabolic Troughs

Enhanced thermal stability



- Comparison of DPO/BP at only 400°C with HELISOL® 5A at 425°C
 - Considerably slower formation of low boiling degradation products
 - Less hydrogen formation (enhanced receiver lifetimes expected)

Advanced Silicon Oil in Parabolic Troughs

Heat transfer fluid	Unit	DPO/BP	HELISOL® 5A
Nominal solar field temperature	°C	393	430
Gross power block efficiency (wet cooling)	%	39.0	40.5
Gross power block efficiency (ACC)	%	37.7	39.2
Nominal specific solar field parasitics	W/m ²	8	6.4
Specific investment solar field	€/m ²	235	235
Specific investment storage	€/kWh	40	33
Specific HTF cost (identical)	€/kg	4	4
Annual HTF replacement rate (identical)	%	2	2
Mean volumetric heat capacity	kJ/(m ³ K)	1871	1397

Benefits over DPO/BP state-of-the-art thermal oil

- Increased performance due to higher live steam temperatures
- Lower storage costs due to increased temperature spread
- LCOE by cost reduction potential of about 5% for different sites and plant sizes



SITEF Project

2016-2017



Supported by:



on the basis of a decision
by the German Bundestag

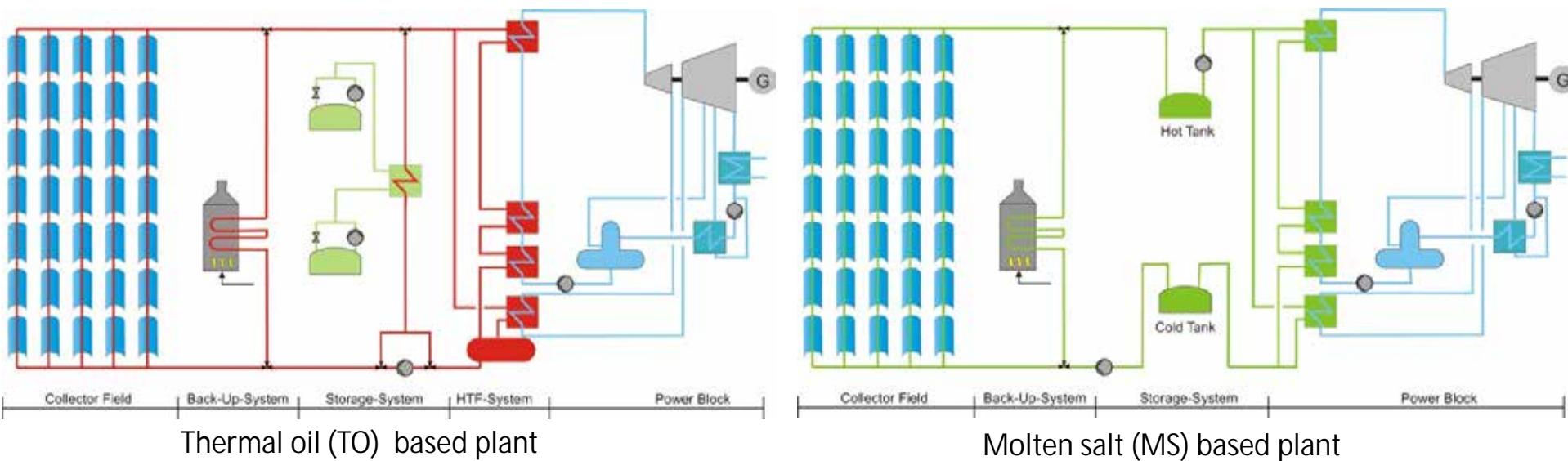


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Molten Salt in Parabolic Trough Power Plants



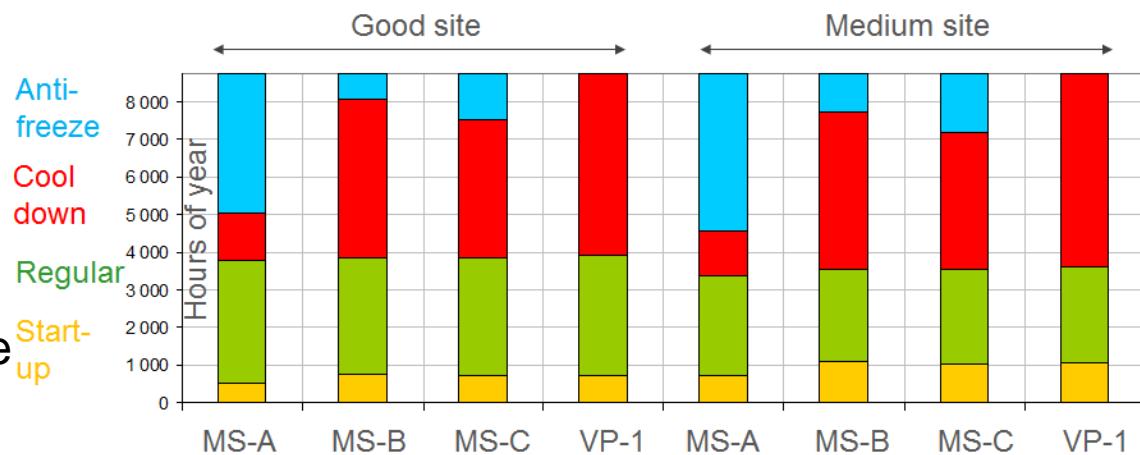
Advantages of the Molten Salt System

- Higher overall system efficiencies due to higher working parameters (up to $565^{\circ}\text{C}/150$ bar instead of $400^{\circ}\text{C}/100$ bar)
- Solar Field and power block fully decoupled
- Lower price for heat transfer fluid (HTF), no need of heat exchangers and additional pumps
- Environmentally friendly heat transfer fluid vs. thermal oil

Parabolic Trough Night operation /w molten salt

- Minimum temperature in solar field must not drop to solidification temperature of the salt
- Choice of salt defines hours of so called anti-freeze operation of a cooled down solar field, e.g. during night and overcast times
- Energy for anti-freeze operation during night and overcast situations is provided by the sun! Part of the thermal energy storage is reserved for anti-freeze and loaded during the day. Only in seldom cases of exception a fossil burner supports.

Salt Mixtures	Decomp. Temperature	Freezing Temperature
MS-A NaK-NO ₃ (Solar Salt)	>550°C	238°C @ 60/40 Mixture
MS-B NaKCa-NO ₃	<500°C	~150°C
MS-C NaKLi-NO ₃	~530°C	~140°C

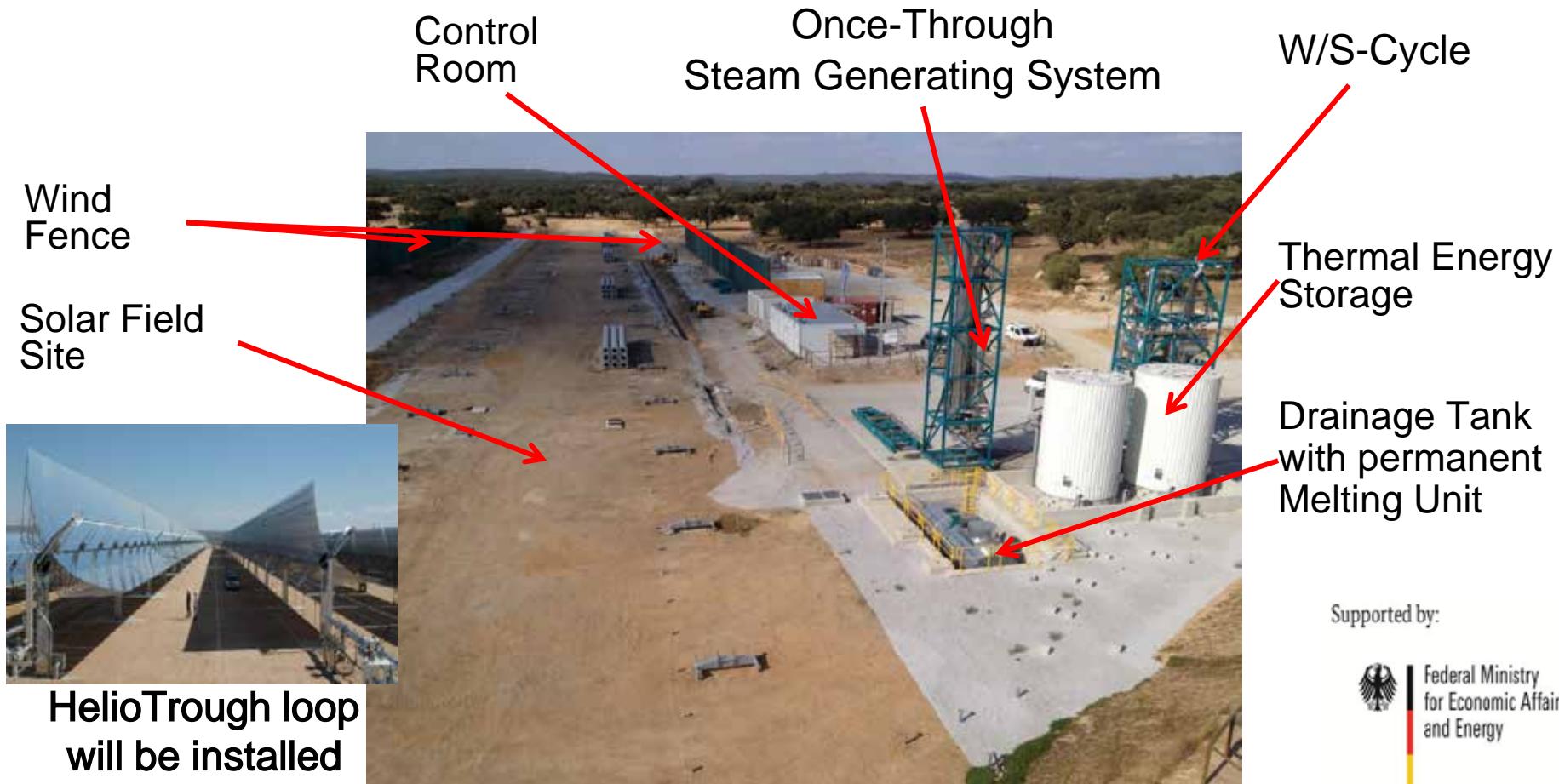


Proof of concept needs to show:

1. Filling and draining of the plant
2. Anti-freeze parasitic load
3. Danger of freezing
4. Blackout scenarios
5. Corrosion at high temperature
6. System performance
7. Flexible connection technology: Proof of functionality and tightness
8. Steam Generating System leakage
9. Maintenance procedures
10. Stability of salt mixtures



DLR's objective in Évora, Portugal: to confute all concerns



Project: HPS2 - High Performance Solar 2
Commissioning of the plant: May 2018

on the basis of a decision
by the German Bundestag

See also: <http://www.dlr.de/sf/en/desktopdefault.aspx/tabcid-10436/20>

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Conclusion

- CSP troughs and towers with large thermal energy storage systems are commercial products today
- In combination with PV, CSP is competitive to 24/7 power from natural gas under favorable conditions
- For solar collectors can replace fuel oil when integrated into a process heat steam supply at grid achieving pay-back periods of < 4 years
- With 5 GW installed the technology is very young and significant further improvement is feasible
- Major future challenges are related to integrate new power cycles that operate at elevated temperatures and require new heat transfer and storage fluids

