

# Modeling and analysis of flux distributions in the two branches of the phosphotransferase system in *Pseudomonas putida* – Supporting information file 1

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## PTS equations and scaling

The complete set of equations for the PTS proteins that are used is given in the following form:

$$\begin{aligned}
 \dot{P}tsP^P &= k_1(PEP PtsP - K_1 Pyr PtsP^P) - k_2(PtsP^P PtsO - K_2 PtsP PtsO^P) \\
 \dot{P}tsO^P &= k_2(PtsP^P PtsO - K_2 PtsP PtsO^P) - k_3(PtsO^P PtsN - K_3 PtsO PtsN^P) \\
 \dot{P}tsN^P &= k_3(PtsO^P PtsN - K_3 PtsO PtsN^P) + k_5(FruB^P PtsN - K_5 FruB PtsN^P) \\
 \dot{F}ruB^P &= k_4(PEP FruB - K_4 Pyr FruB^P) - k_5(FruB^P PtsN - K_5 FruB PtsN^P) \\
 &- r_{fru}
 \end{aligned} \tag{1}$$

Introducing the conservation equation  $X + X^P = X_0$  and scaling with  $x = X^P/X_0$ ,  $\tau = k_1 Pyr$  leads to (prime indicates derivative with respect to  $\tau$ ):

$$\begin{aligned}
 ptsP^{P'} &= \frac{PEP}{Pyr} (1 - ptsP) - K_1 ptsP^P \\
 &- \frac{k_2 PtsO_0}{k_1 Pyr} (ptsP^P (1 - ptsO^P) - K_2 ptsP ptsO^P)
 \end{aligned}$$

$$\begin{aligned}
ptsO^{P'} &= \frac{k_2 PtsP_0}{k_1 Pyr} (ptsP^P (1 - ptsO^P) - K_2 (1 - ptsP^P) ptsO^P) \\
&\quad - \frac{k_3 PtsN_0}{k_1 Pyr} (ptsO^P (1 - ptsN^P) - K_3 (1 - ptsO^P) ptsN^P) \\
ptsN^{P'} &= \frac{k_3 PtsO_0}{k_1 Pyr} (ptsO^P (1 - ptsN^P) - K_3 (1 - ptsO^P) ptsN^P) \\
&\quad + \frac{k_5 FruB_0}{k_1 Pyr} (fruB^P (1 - ptsN^P) - K_5 (1 - fruB^P) ptsN^P) \\
fruB^{P'} &= \frac{k_4}{k_1} \left( \frac{PEP}{Pyr} (1 - fruB^P) - K_4 fruB^P \right) \\
&\quad - \frac{k_5 PtsN_0}{k_1 Pyr} (fruB^P (1 - ptsN^P) - K_5 (1 - fruB^P) ptsN^P) \\
&\quad - \frac{r_{fru}}{k_1 Pyr FruB_0}
\end{aligned} \tag{2}$$

The dimensionless system has two inputs (PEP/pyruvate ratio and scaled fructose uptake rate), 5 equilibrium constants  $K_i$  and seven kinetic parameters  $\alpha_j$ :

$$\begin{aligned}
\alpha_1 &= \frac{k_2 PtsO_0}{k_1 Pyr} & \alpha_2 &= \frac{k_2 PtsP_0}{k_1 Pyr} & \alpha_3 &= \frac{k_3 PtsO_0}{k_1 Pyr} \\
\alpha_4 &= \frac{k_3 PtsN_0}{k_1 Pyr} & \alpha_5 &= \frac{k_5 FruB_0}{k_1 Pyr} & \alpha_6 &= \frac{k_4}{k_1} & \alpha_7 &= \frac{k_5 PtsN_0}{k_1 Pyr}
\end{aligned} \tag{3}$$

Note, that in the most cases considered in the manuscript, a number of rates are zero. In these cases, scaling does not play any role, since the equilibrium is invariant. The most important case for the complete set is growth of the wild type strain on CAA plus fructose. Here, the individual rates are not zero. For the equations for  $ptsO^P$  and  $ptsN^P$ , factors  $\alpha_2$ ,  $\alpha_3$ ,  $\alpha_4$  are assumed to be in the same order of magnitude, since all have identical structures. For the equations for  $ptsP^P$  and  $fruB^P$  different expressions appear. Since the concentration of a metabolite is far higher than the one of a protein, a factor 100 is used here that relates the values for  $PEP/Pyr$  and  $\alpha_2$ ; and  $\alpha_6$  and  $\alpha_7$ , respectively. To obtain a scaled value for the uptake rate  $r_{fru}$  the following rough estimation was performed: The value of the fructose uptake rate is  $r_{fru} = 0.08$  mmol/gDW h. Parameter  $k_1$  is  $2 \cdot 10^5 1/(\mu\text{mol/gDW h})$  [Kremling et al., Analysis of global control of *Escherichia coli* carbohydrate uptake, BMC Systems Biology 42, 2007], the concentration of pyruvate in the order of  $10 \mu\text{mol/gDW}$  [Sauter and Gilles, Modeling and experimental validation of the signal transduction via the *Escherichia coli* sucrose phosphotransferase system, Journal of Biotechnology 110, 2004; Bettenbrock et al., A quantitative approach to catabolite repression, JBC 281, 2006] and the

concentration of a PTS protein in the order of  $1 \cdot 10^{-1} \mu\text{mol/gDW}$  [Bettenbrock et al., A quantitative approach to catabolite repression, JBC 281, 2006; J. Rohwer et al., Understanding glucose transport by the bacterial phosphoenolpyruvate: glucose phosphotransferase system on the basis of kinetic measurements *in vitro*, JBC 275, 2000] . Based on this values, a value of  $r'_{fru} = 0.001$  was chosen.

For growth on CAA plus fructose, the complete set of equations has to be solved to determine the steady state degree of phosphorylation. The assumption of a steady state is reasonable since the phosphoryl transfer between the PTS proteins runs on a much faster time scale than metabolic reactions. Taking into account that some of the values for  $\alpha_i$  are in the same order of magnitude, and with the values from above, the following set of equations is solved with MATLAB (.m files are available on request):

$$\begin{aligned}
0 &= r'_1 - \frac{1}{100} r'_2 \\
0 &= r'_2 - r'_3 \\
0 &= r'_3 + r'_5 \\
0 &= r'_4 - \frac{1}{100} r'_5 - r'_{fru}
\end{aligned} \tag{4}$$

## Kinetic parameters

Based on the available data not all parameters could be calculated. Therefore, the following strategy was chosen: Parameter  $K_3$  was first fixed to  $K_3 = 1$ . For growth in CAA the PEP/pyruvate ratio  $pp$  was set to 1. Considering the wild type, the conditions given in the main text and the available experimental data, the following condition that allows to determine  $K_1$  holds true: The equations were written in such a form that the unknowns,  $PtsP^P$  or  $PtsO^P$ , were eliminated:

$$PtsP^P = \frac{K_2 K_3}{1 - PtsP^P (1 - K_2 K_3)} = \frac{pp}{K_1 + pp} \tag{5}$$

Afterwards, the same equation is used to determine the PEP/pyruvate ratio  $pp$  for growth on CAA plus fructose. The product  $K_4 \cdot K_5$  can be determined from the fact that for both branches, the equilibrium constant must be the same. Finally, considering growth on CAA plus fructose for the PtsP mutant,  $r_3 = r_5 = 0$  and hence  $r'_4 = r'_{fru}$  allows to calculate  $K_5$ . With the parameters so far, a value for  $K_2$  was chosen in such a way that it fits the data at best. It was observed that there is a saturation behavior when varying  $K_2$ , that is, larger values of  $K_2$  have no influence on the simulation results. Finally the influence of the

choice  $K_3 = 1$  was analyzed. It turns out that  $K_3$  could be changed only in a small range. Therefore  $K_3 = 1$  was the final fixing. The resulting values are as follows (all values are dimensionless):

$K_1$	$K_2$	$K_3$	$K_4$	$K_5$
0.02	1.0	1.0	$3.12 \cdot 10^{-5}$	654.6

Figure 1 shows the influence of varying parameters  $K_2$  and the PEP/pyruvate ratio since these values are set a priori. The default condition is marked with a black square. The colors represent values of the objective function (least square approach):

$$\Phi = \sum \frac{(y_{Mi} - y_i)^2}{\sigma^2} \quad (6)$$

with  $y_{Mi}$  measured values,  $y_i$  simulated values and  $\sigma$  the standard deviation (values are given in Table 2 in the main text). The model can be assessed by comparing the values of  $\Phi$  with values given from a  $\chi^2$  distribution. For the calculation shown in Figure 1, 10 data points are considered and five parameters are estimated ( $K_i$  and PEP/pyruvate ratio; note that not all  $K_i$  value could be chosen independently), so the range for  $\chi^2$  is given by 5 degree of freedom. The respective valid interval is therefore between 0.83 and 12.83.

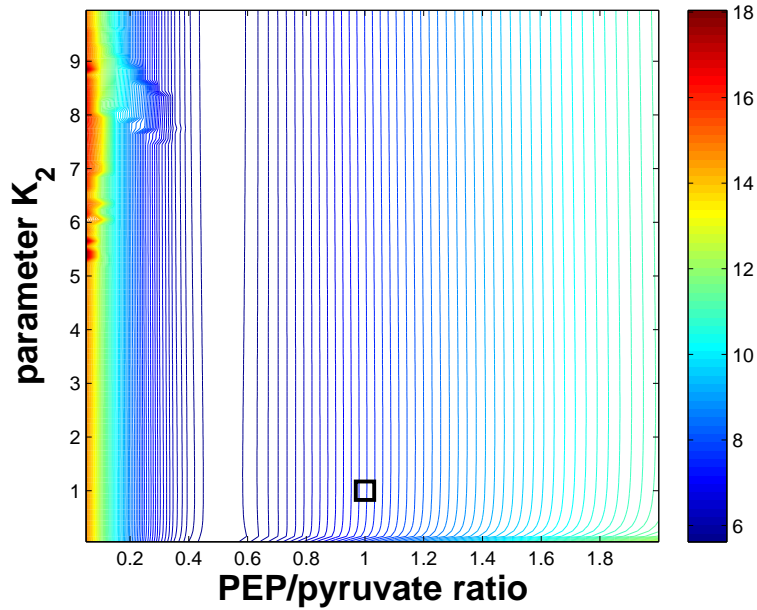


Figure 1: Contour plot for  $\Phi$  in dependence on  $K_2$  and the PEP/pyruvate ratio. The black square indicates the two values used in the calculations.

As can be seen, parameter  $K_2$  has only marginal influence on the objective function. The PEP/pyruvate ratio could be changed in reasonable borders without leaving the interval given by the  $\chi^2$  distribution. The

black square indicates the two values used in the calculations.

### Kinetics for the PEP synthase $r_c$ and gluconeogenic reaction $r_d$

Based on power law kinetics the following results are obtained for the two reactions:

$$\begin{aligned} r_c &= k_c Pyr^{n_c} & \text{with } k_c = 1; n_c = 1 & \text{ are set} \\ r_d &= k_d PEP^{n_d} & \text{with } k_d = 2.73; n_d = 0.30 & \end{aligned} \quad (7)$$

Based on the values for the flux variability analysis, the value of  $k$  in Figure 8 might change. For the default condition  $k = 0.34$ . Since  $k$  is defined as  $k = \frac{\Delta r_b}{\Delta r_a}$  it increases for larger values of  $\Delta r_b$  and smaller values of  $\Delta r_a$  and decreases for smaller values of  $\Delta r_b$  and larger values of  $\Delta r_a$ . Taking the values from Table 3 different values for  $\Delta r_a$  and  $\Delta r_b$  could be determined; the extreme conditions lead to values  $k_{max} = 0.47$  and  $k_{min} = 0.22$ . These values are used in the calculation. The confidence region is shown in Figure 9 with dashed lines.