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Highly crosslinked, chlorine-tolerant polymer network entwined graphene oxide membrane for water desalination

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Supplementary Information

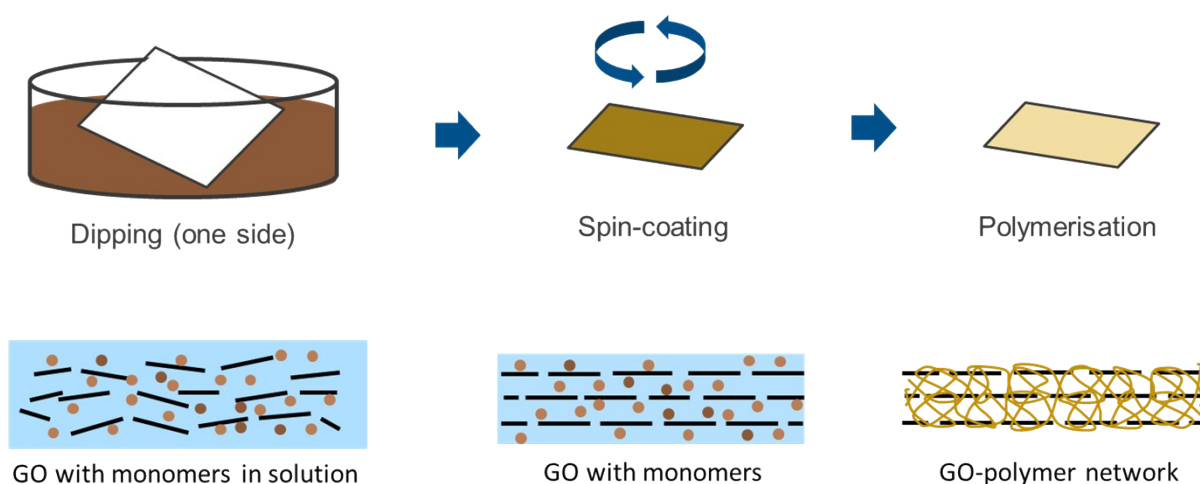


Fig. S1 Schematic representation of fabrication of polymer network entwined GO thin-film composite membrane.

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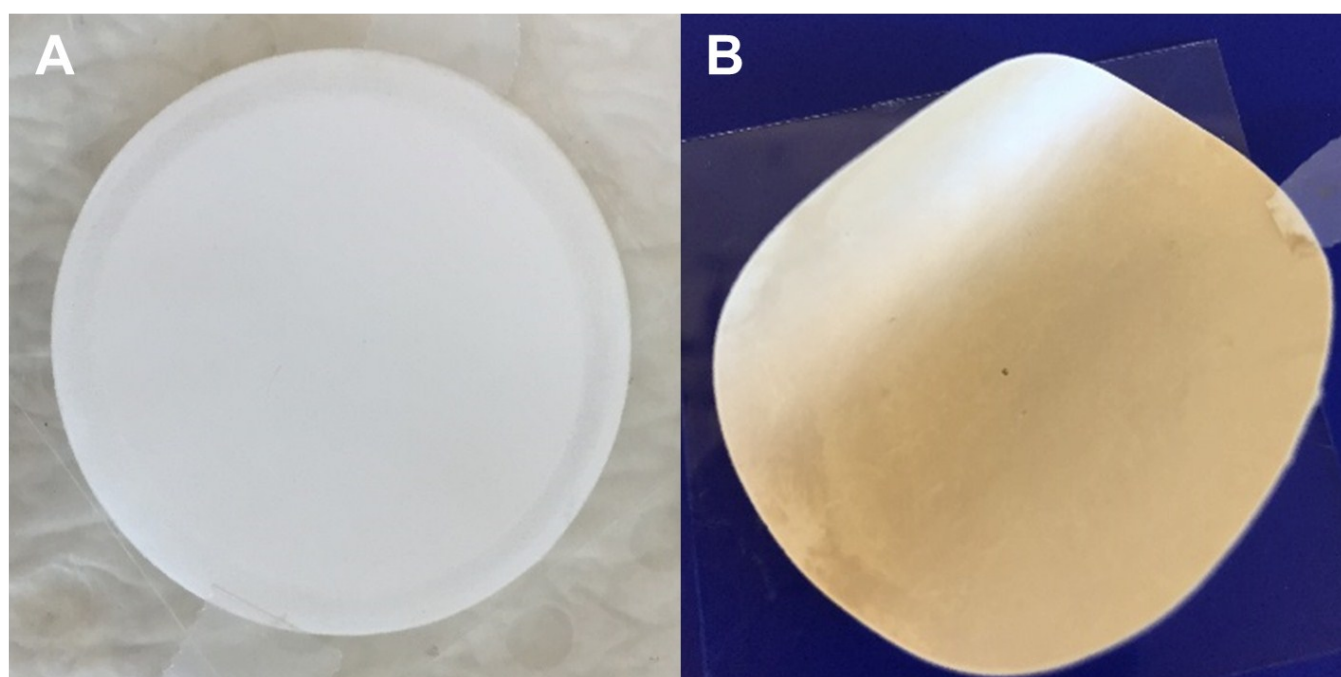
† Footnotes relating to the title and/or authors should appear here.

Electronic Supplementary Information (ESI) available: [details of any supplementary information available should be included here]. See DOI: 10.1039/x0xx00000x

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Table S1 Detailed quantities of components in the precursor solution for spin-coating

Samples	Monomers (mg)			Water (ml)	GO (mg)	GO conc. (mg/ml)	GO/polymer ratio (wt%)
	NIPAM	MBA	APS				
GO-P61					3.4	0.34	4.5
GO-P65					4.8	0.48	6.3
GO-P72	38	38	7	10	9.5	0.95	12.5
GO-P79					19	1.9	25.0
GO-P87					28.5	2.85	37.5
GO-P95					38	3.8	50.0

**Fig. S2** Photos of (A) a Nylon substrate, and (B) a GO-polymer composite membrane (GO-P61).

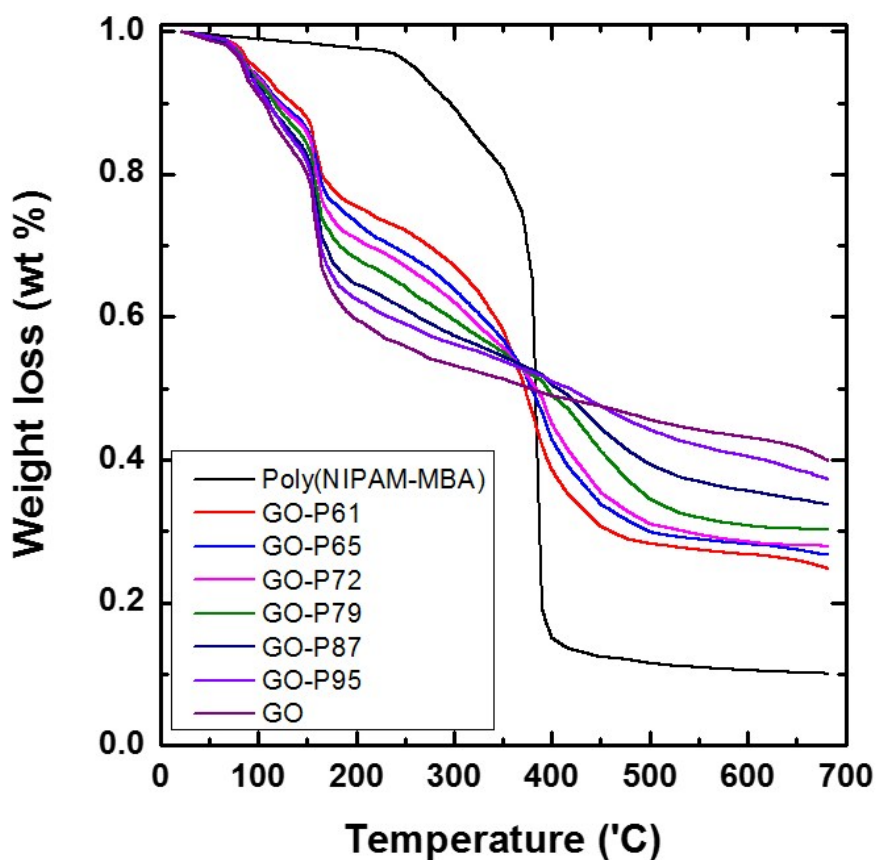


Fig. S3 Thermogravimetric analysis (TGA) curves of GO-polymer composites with different GO/polymer ratios.

Poly(*N*-isopropylacrylamide-*co-N,N'*-methylene-bis-acrylamide) are thermally stable until around 250 °C and dramatically decomposed after 350 °C. Otherwise, there is a serious weigh loss between 100 °C and 200 °C on GO from a decomposition of hydroxyl groups on GO. GO-polymer ratio was confirmed by comparison of weight change between 100 °C and 250 °C.

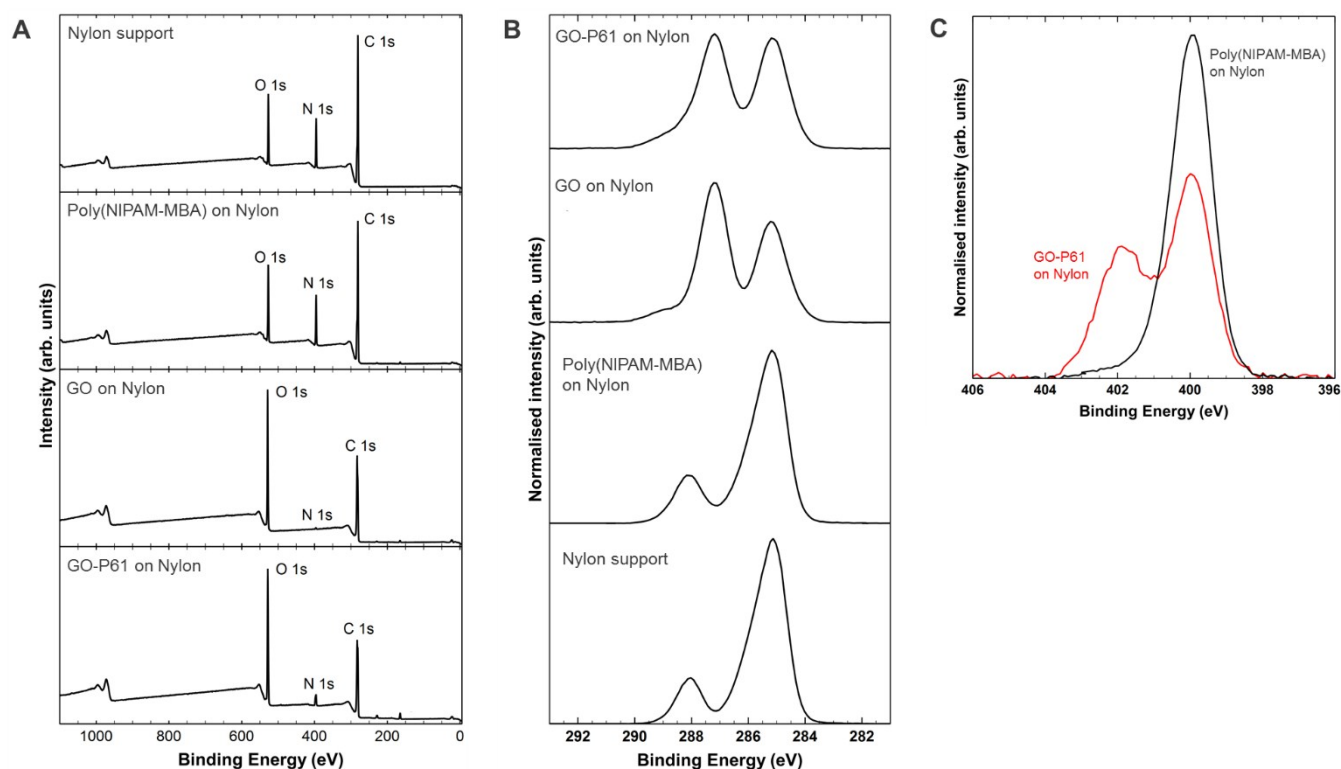


Fig. S4 X-ray photoelectron spectroscopy (XPS) spectra (a) survey spectrum series, (b) selected, representative C 1s spectra of untreated and modified Nylon support samples, and (c) selected, representative N 1s spectra overlay of polymer coated Nylon filter with (GO-P61) and without GO (poly(NIPAM-MBA)).

XPS analysis confirms GO on Nylon as the N signal is suppressed significantly and N/O ratio has dropped as compared with raw Nylon support.¹ In the C 1s spectra (**Fig. S4B**), spectra are normalised to total peak area and charge corrected using a binding energy reference value of 285 eV for aliphatic hydrocarbon. Intensity in the region 288 eV is associated with amides, as expected for the Nylon support and poly(NIPAM-MBA) coated Nylon support samples, where the peak shape is characteristic of a polyamide. The introduction of intensity in the region of 287 eV for the GO treated samples is associated with C-O.² For the N 1s spectra (**Fig. S4C**), the addition of GO to the poly(NIPAM-MBA) results in intensity in the region 402 eV, which is associated with N⁺ groups; this suggests there is a charge interaction between the PNIPAM and GO.³

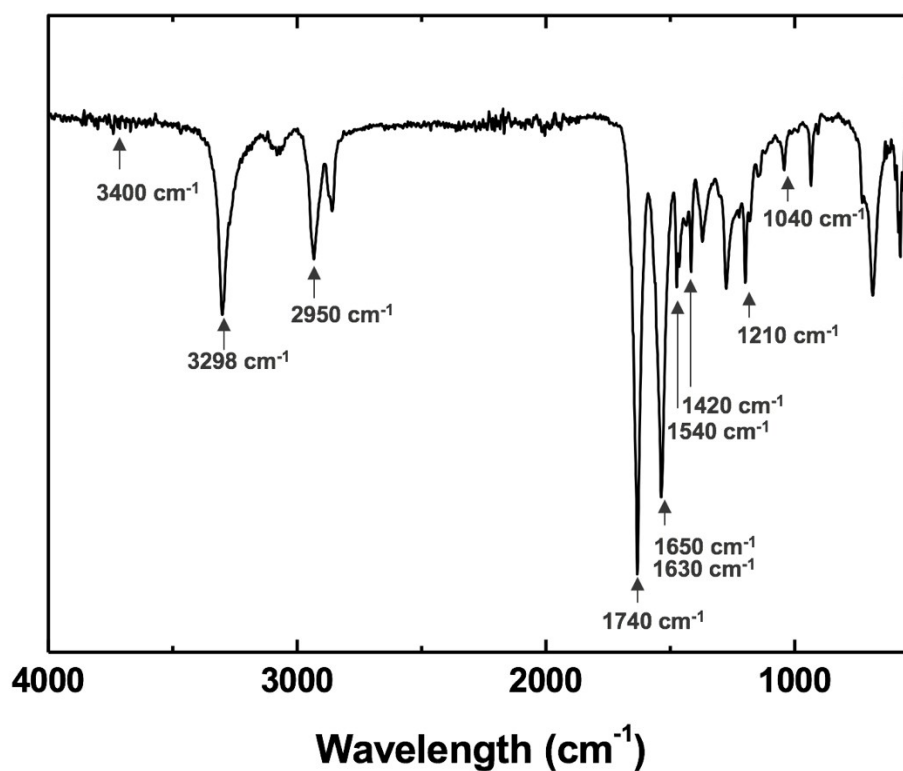


Fig. S5 Attenuated total reflection-Fourier transform infrared (ATR-FTIR) spectrum of a GO-polymer thin-film composite membrane (GO-P61).

ATR-FTIR spectrum of a GO-polymer shows combined characteristics of GO and poly(NIPAM-MBA). The main peaks are as follows: 3298 cm⁻¹ (secondary amide N-H stretching), 2950 cm⁻¹ (-CH₃ asymmetric stretching), 1740 cm⁻¹ (secondary amide C=O stretching, 1650 cm⁻¹ (secondary amide C=O stretching, aka amide I bond), and 1540 cm⁻¹ (C-N stretching) for poly(NIPAM-MBA).^{4,5} 3400 cm⁻¹ (O-H stretching), at 1630 cm⁻¹ (skeletal vibrations from unoxidized graphitic domains), 1420 cm⁻¹ (C=C aromatic ring) 1210 cm⁻¹ (C-O-C stretching), and 1040 cm⁻¹ (C-O stretching) for GO.^{5,6} GO peaks are relatively weak as compared with poly(NIPAM-MBA) because of coverage of poly(NIPAM-MBA).

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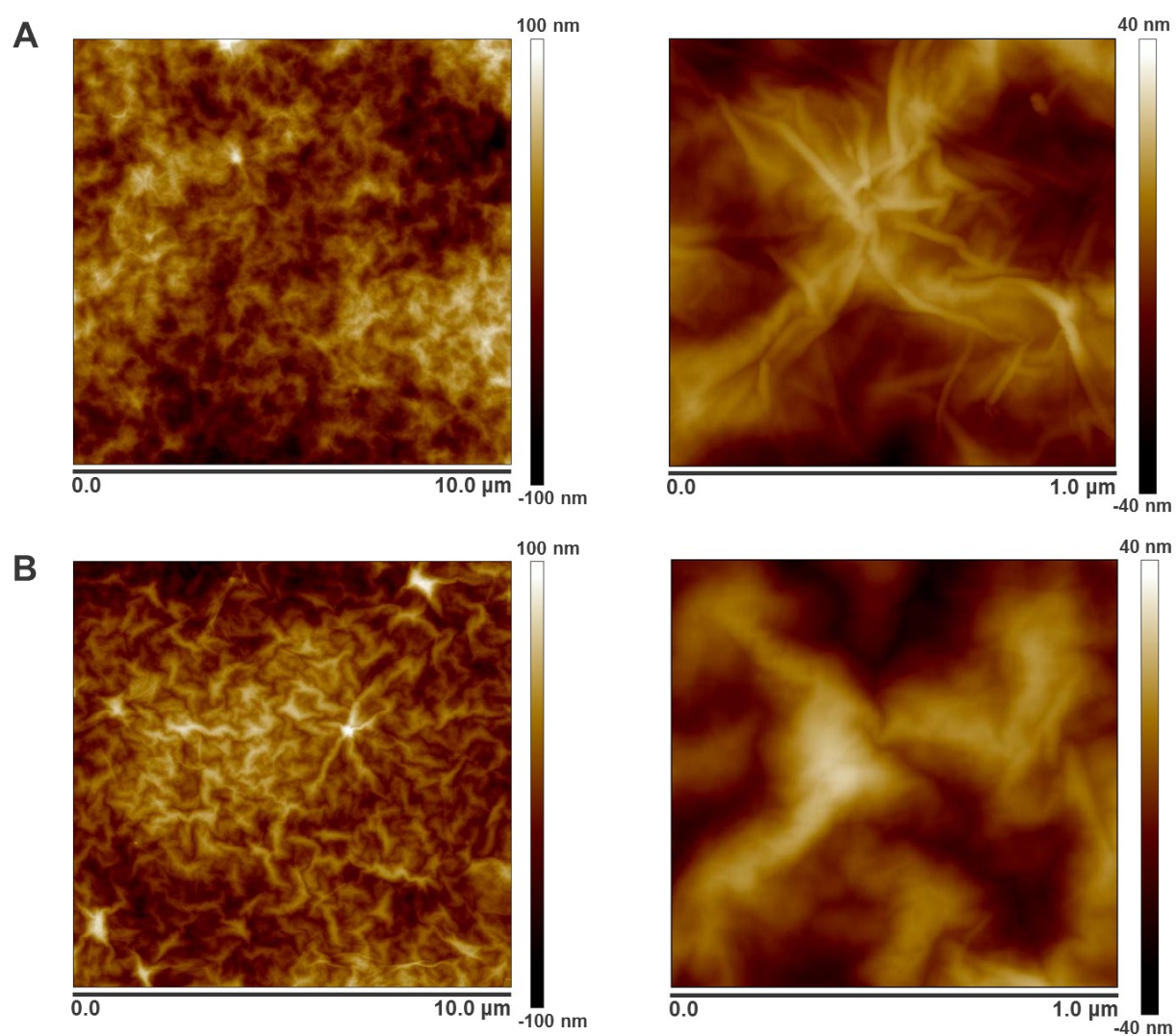


Fig. S6 2D AFM images of (A) a GO-polymer thin-film composite membrane (GO-P61), and (B) a layered GO membrane prepared by spin-coating.

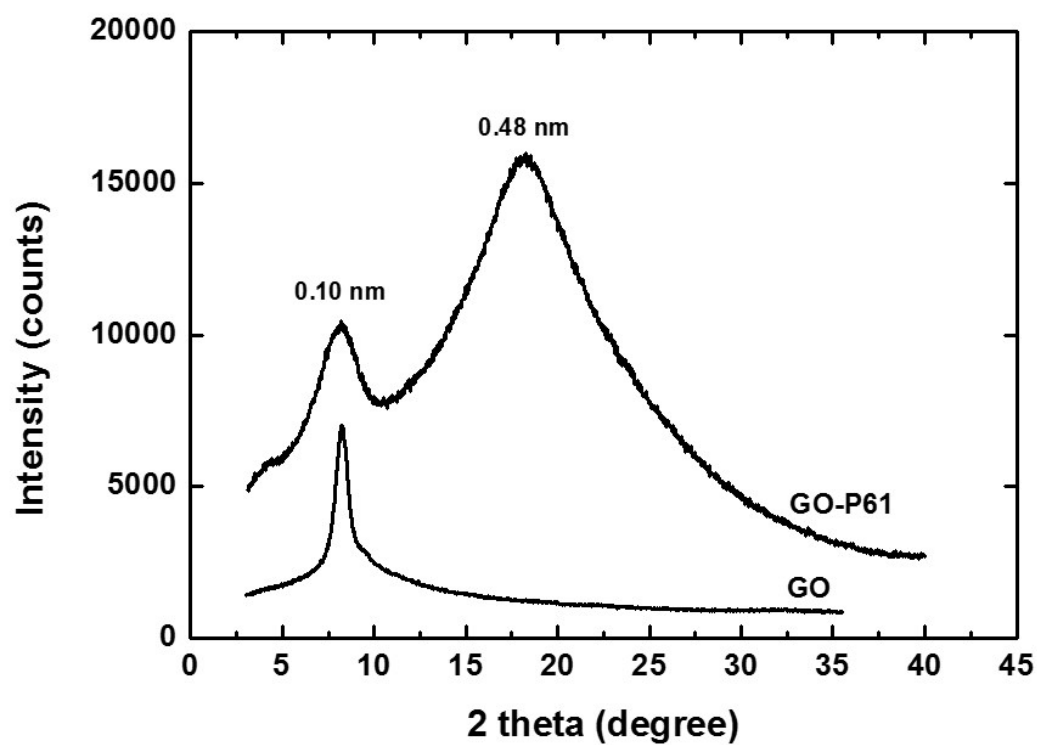


Fig. S7 XRD patterns of a GO and a GO-polymer thin-film composite membrane (GO-P61).

The d-spacing values for the peaks at 8.5° and 18.0° were calculated using Bragg's equation to be 1.04 nm and 0.48 nm, respectively. Because poly(NIPAM-MBA) is amorphous, the d-spacing values should correspond to the interlayer spacing of GO nanosheets. The weak peak at 8.5° is similar to that observed in the pure GO laminate.⁷

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* FO performances characterization

The water flux (J_w , L m⁻² h⁻¹) was calculated by:

$$J_w = \frac{\Delta w}{s t} \quad (1)$$

where Δw (L) is the volume change of the feed solution, s (m²) is the effective membrane area and t (h) is the filtration time.

The reverse salt flux (J_s , g m⁻², h⁻¹) was calculated by

$$J_s = \frac{C_t V_t - C_0 V_0}{s t} \quad (2)$$

where C_0 (g/L) and V_0 (L) are the initial solute concentration and the initial volume of the feed, respectively, while C_t (g/L) and V_t (L) are the solute concentration and the volume of the feed over a running time t (h). The solute concentration of the feed solution was determined from the conductivity of the solution.

The FO salt rejection (%) was calculated by

$$R = \left(1 - \frac{C_p}{C_f}\right) \times 100 = \left(1 - \frac{J_{s,p}/J_{w,p}}{C_f}\right) \times 100 \quad (3)$$

where C_p (g/L) and C_f (g/L) are the salt concentration at permeate and feed.

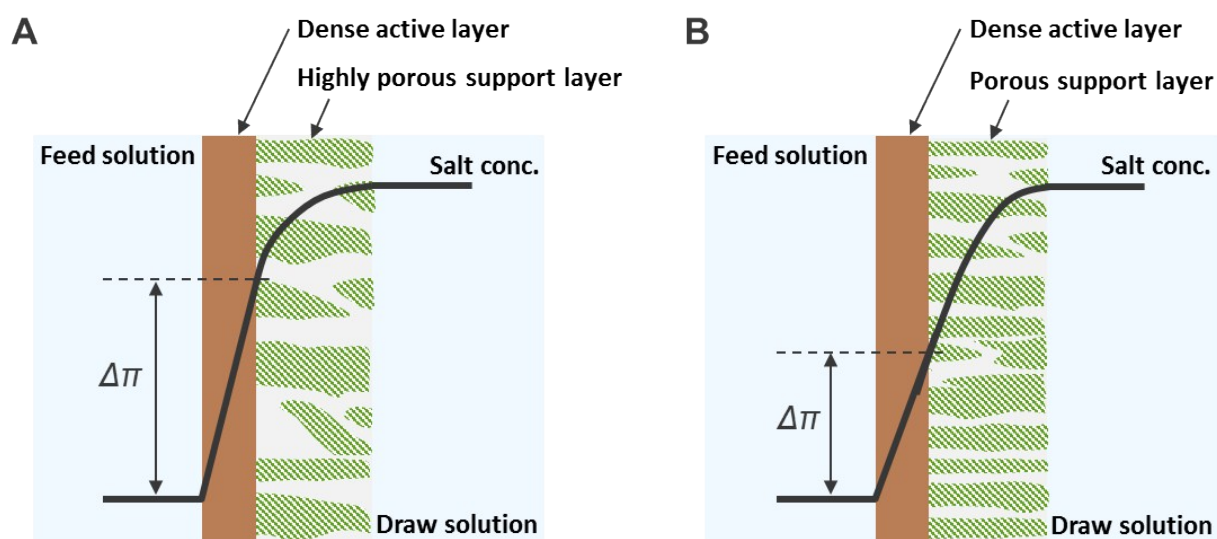


Fig. S8 Osmotic pressure difference of FO composite membranes (A) when a highly porous support was used, and (B) when a less porous support was used.

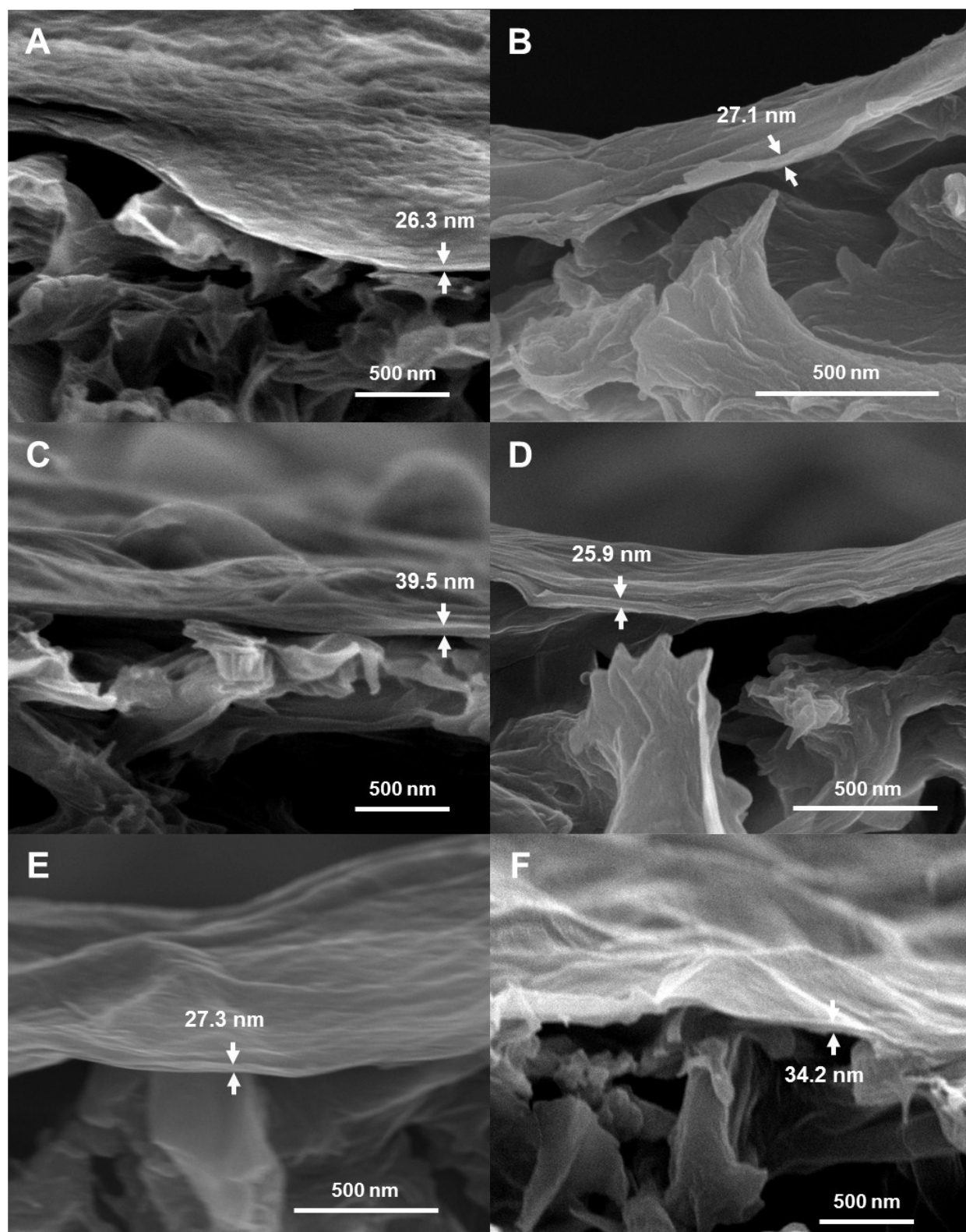


Fig. S9 Cross-sectional SEM images of GO-polymer composite membranes (A) GO-P61, (B) GO-P65, (C) GO-P72, (D) GO-P79, (E) GO-P87, and (F) GO-P95.

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